



# Faculty of Automotive and Construction Machinery Engineering

WARSAW UNIVERSITY OF TECHNOLOGY

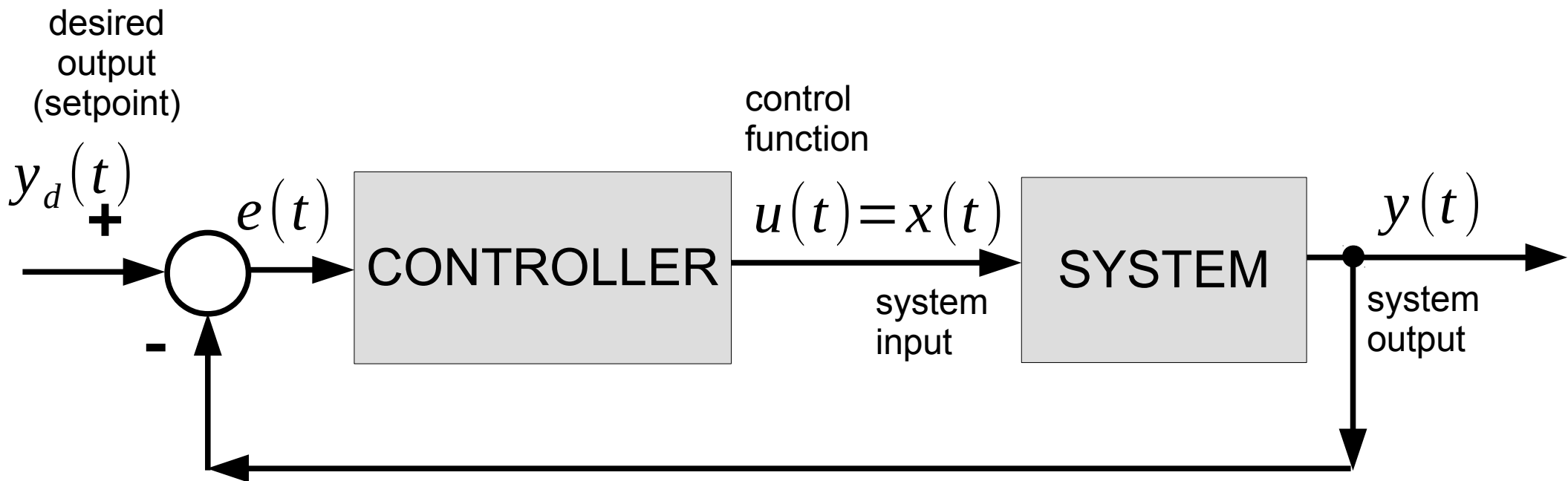
## *Theory of Machines and Automatic Control* Winter 2019/2020

**Lecturer: Sebastian Korczak, PhD Eng.**

# Lecture 12

PID controller.  
Stability.

# Closed loop control



# P, I and D controllers transfer functions

<b>Controller</b>	<b>Transfer function</b>
Proportional (P)	$k_P$
Integral (I)	$\frac{1}{T_i s}$
Ideal derivative (D)	$T_d s$
Real derivative (D)	$\frac{T_d s}{T s + 1}$

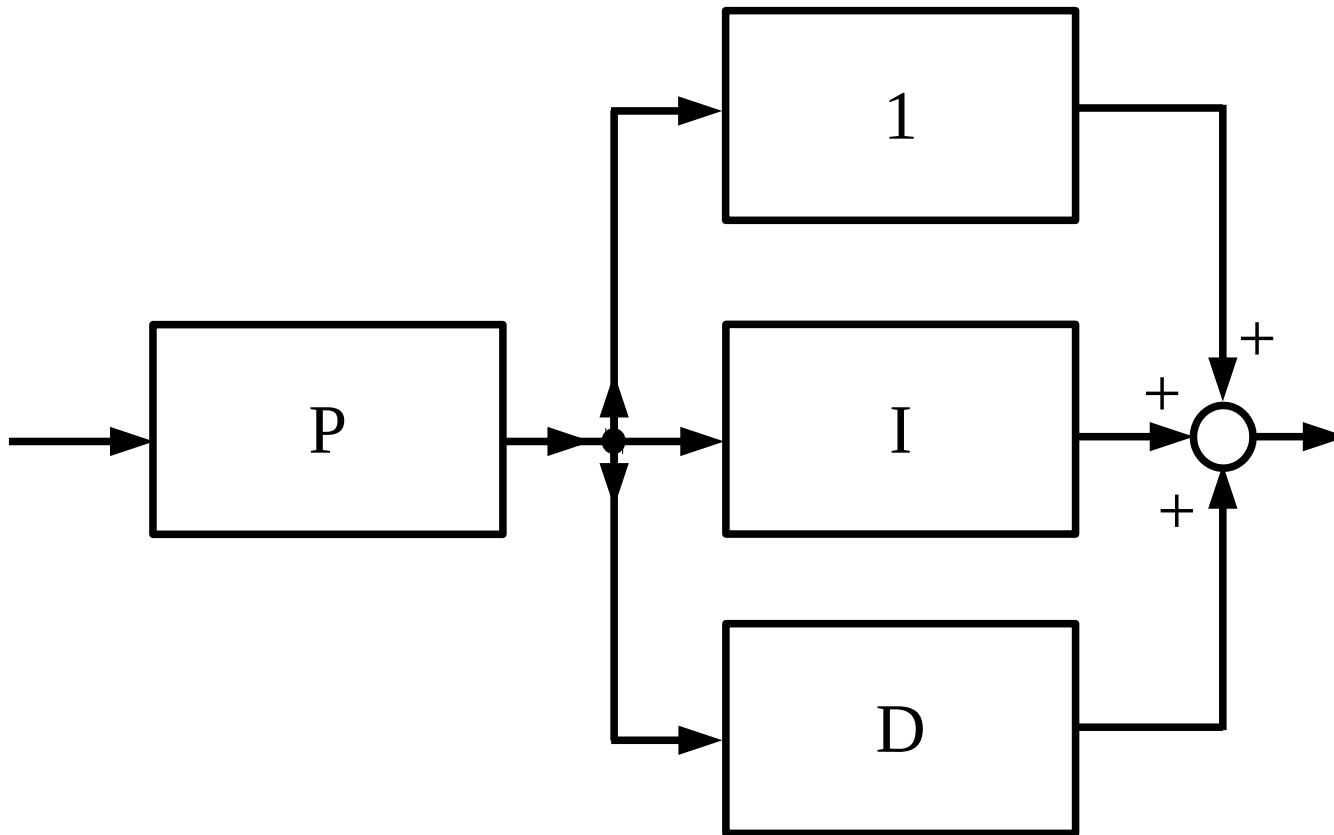
# PID controllers transfer functions

<b>Controller</b>	<b>Transfer function</b>
Proportional-integral-derivative (PID) <u>in standard form</u> with ideal derivative	$k_P \left( 1 + \frac{1}{T_i s} + T_d s \right)$
Proportional-integral-derivative (PID) <u>in parallel form</u> with ideal derivative	$k_P + k_i \frac{1}{s} + k_d s$

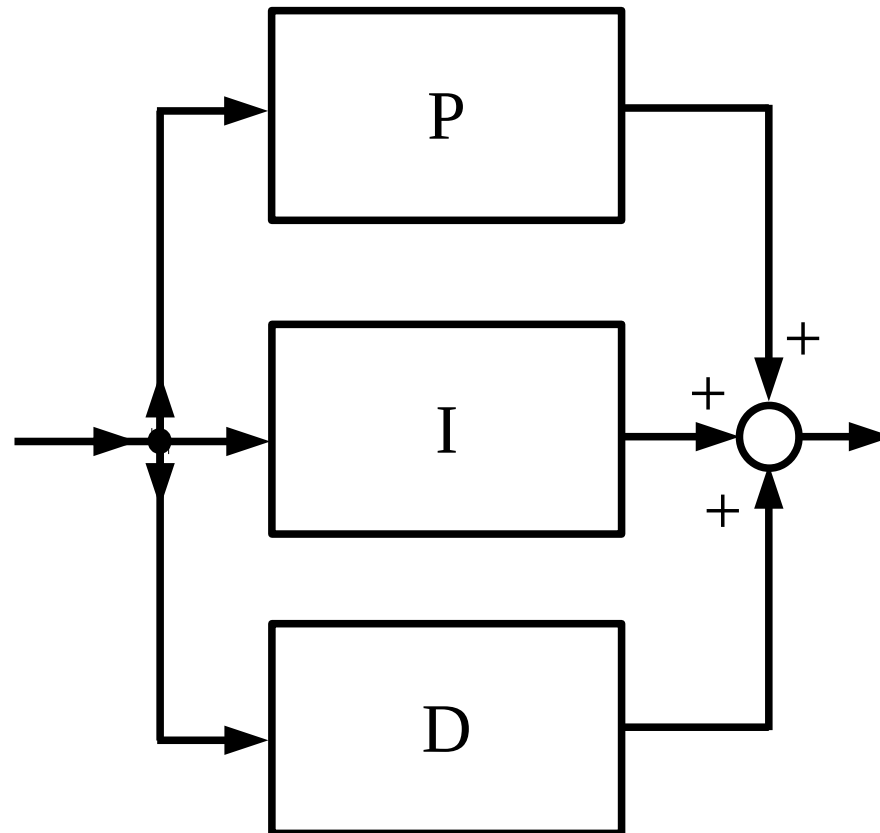
# PID controllers transfer functions

<b>Controller</b>	<b>Transfer function</b>
Proportional-integral-derivative (PID) <u>in standard form</u> with real derivative	$k_P \left( 1 + \frac{1}{T_i s} + \frac{T_d s}{Ts + 1} \right)$
Proportional-integral-derivative (PID) <u>in parallel form</u> with real derivative	$k_P + k_i \frac{1}{s} + k_d \frac{s}{Ts + 1}$

# PID CONTROLLER standard form

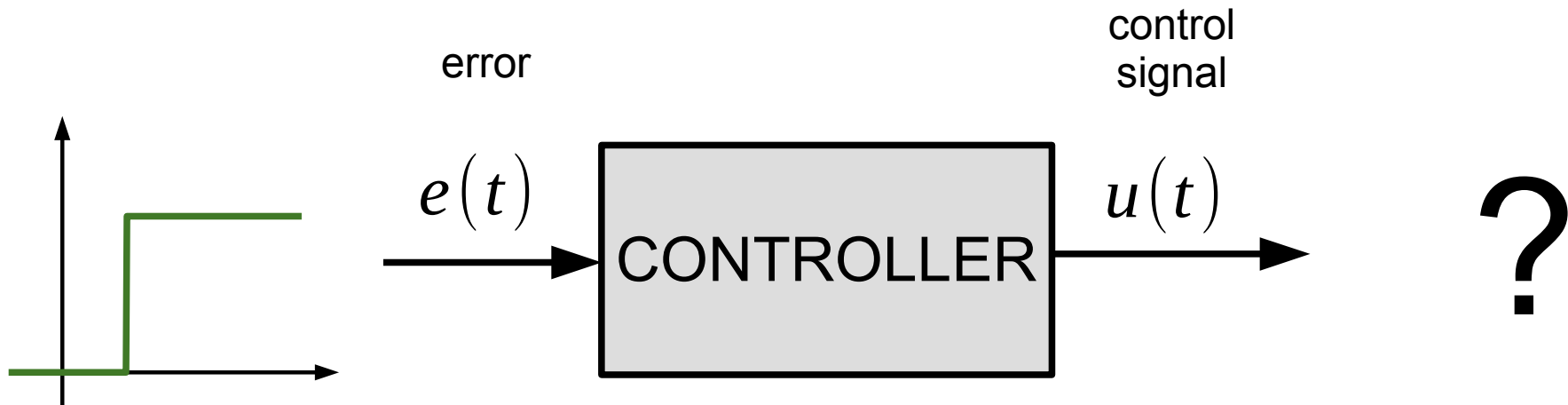


# PID CONTROLLER parallel form



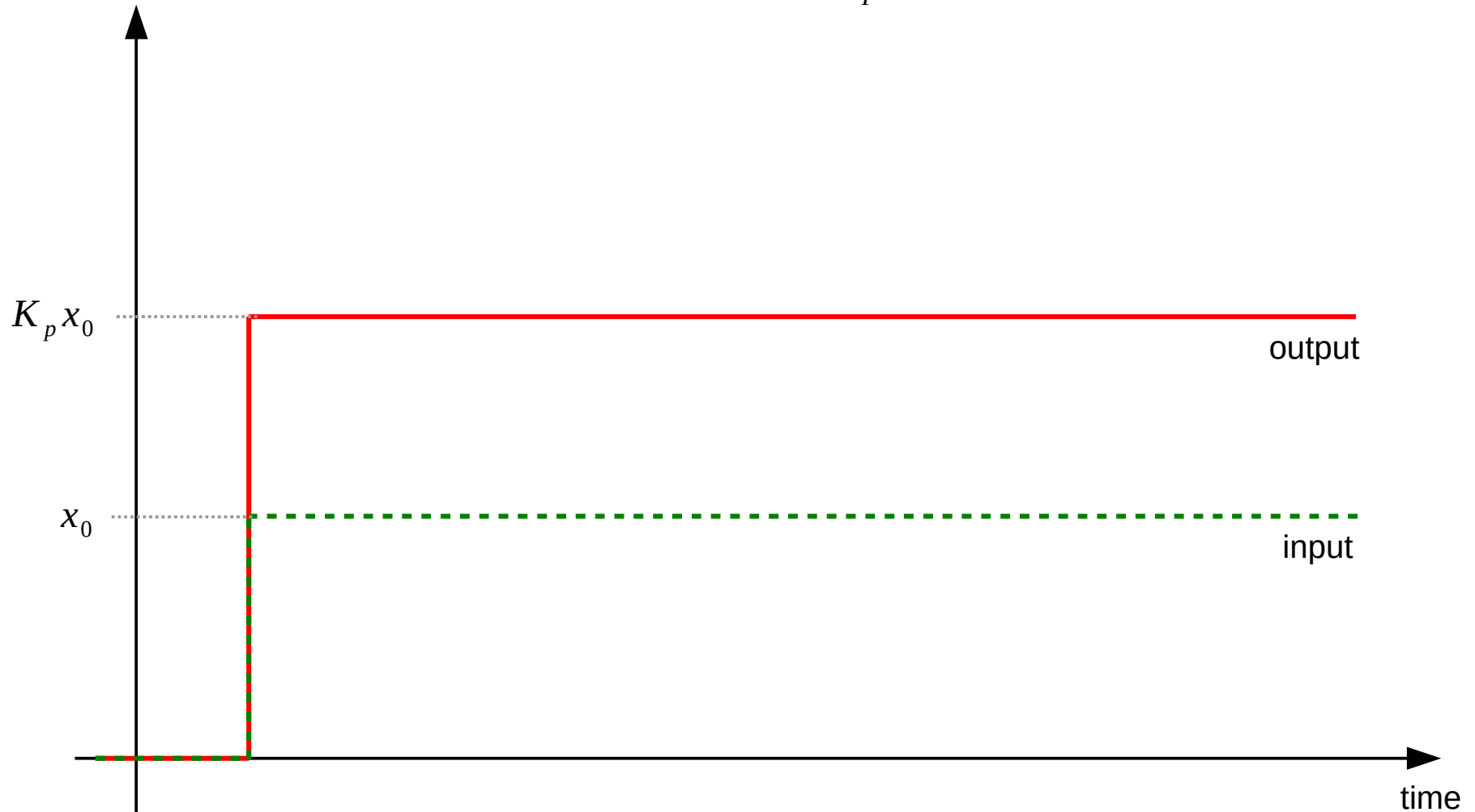


# PID CONTROLLER step responses



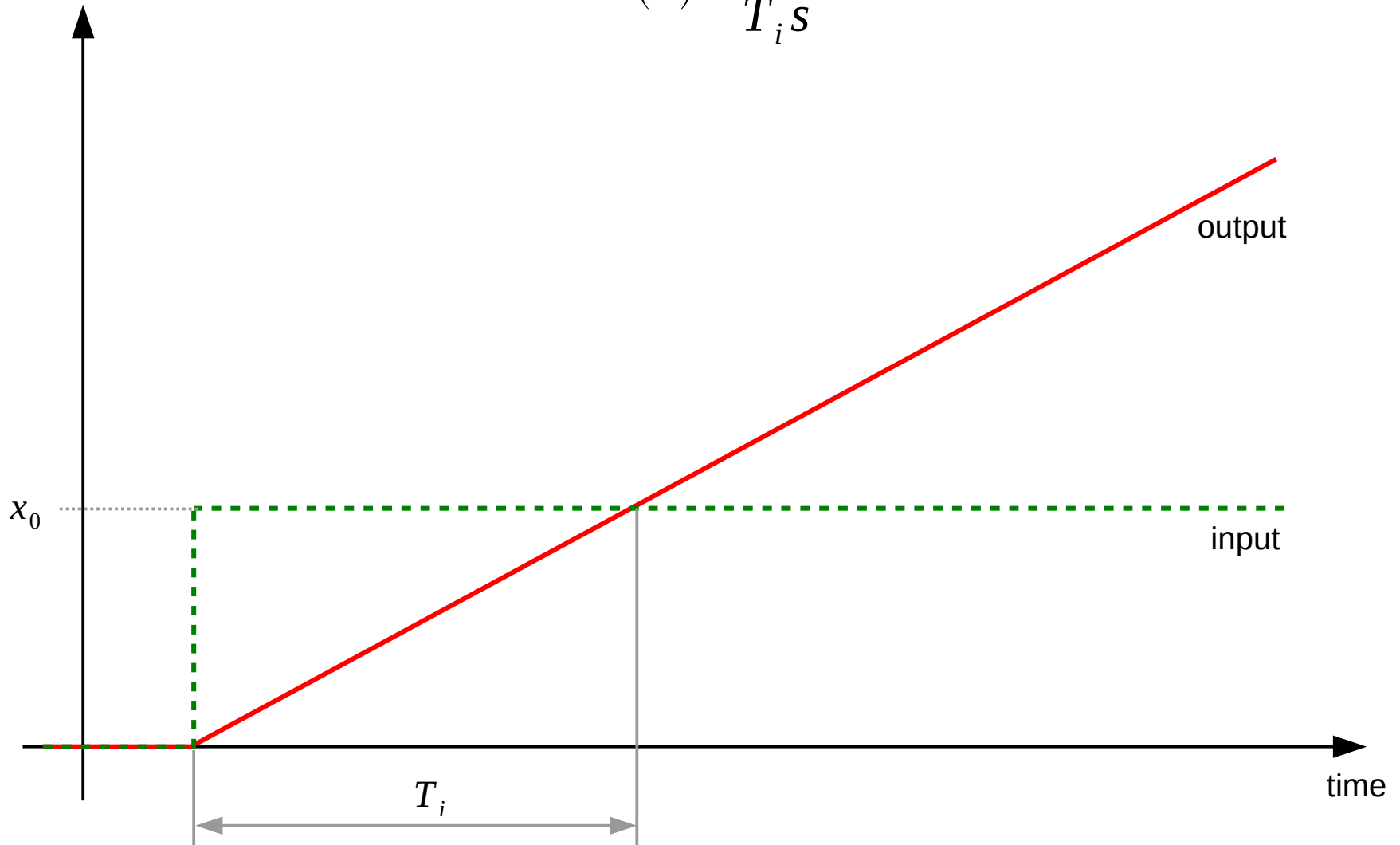
# P - CONTROLLER

$$H(s) = K_p$$



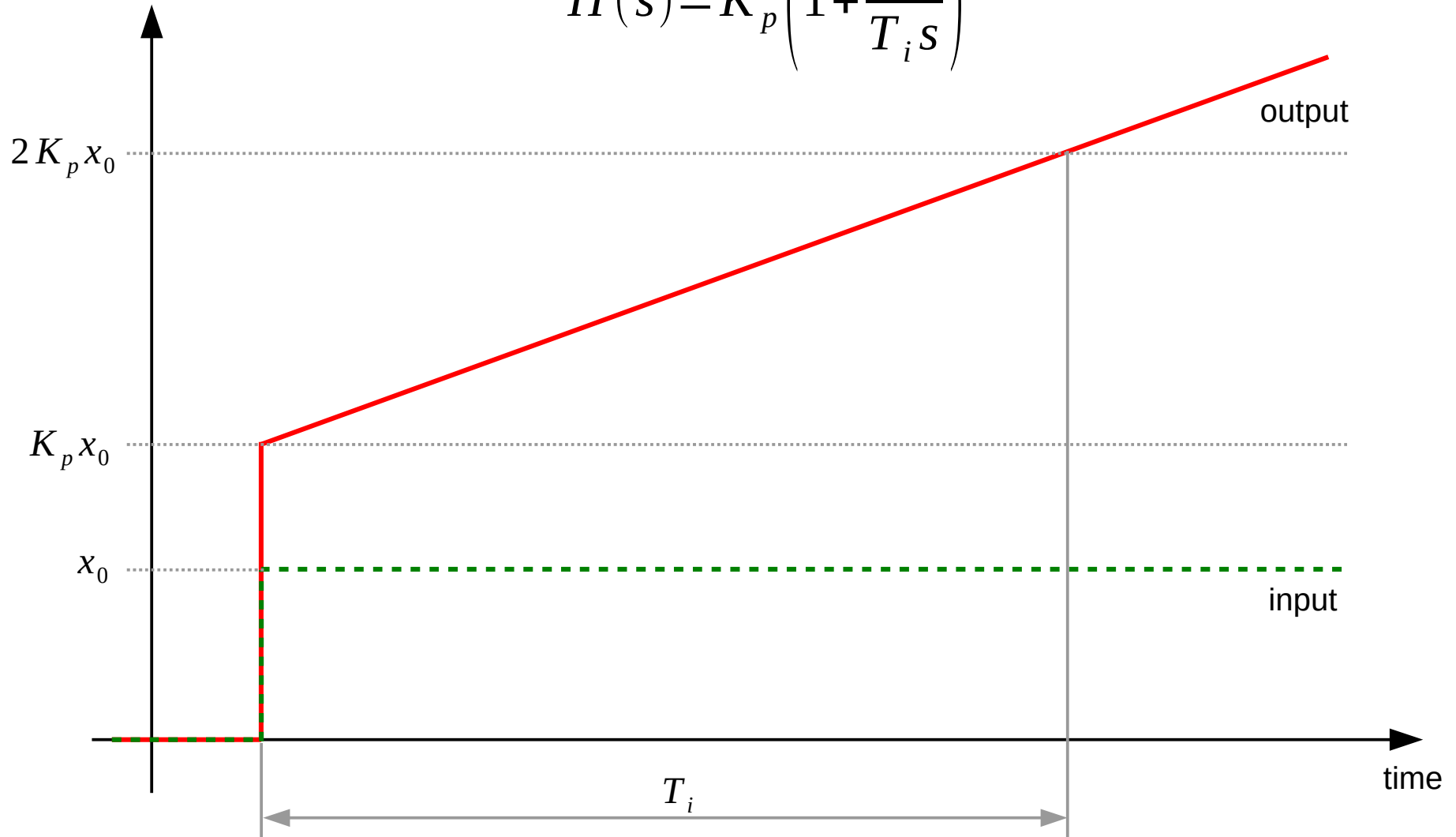
# I - CONTROLLER

$$H(s) = \frac{1}{T_i s}$$



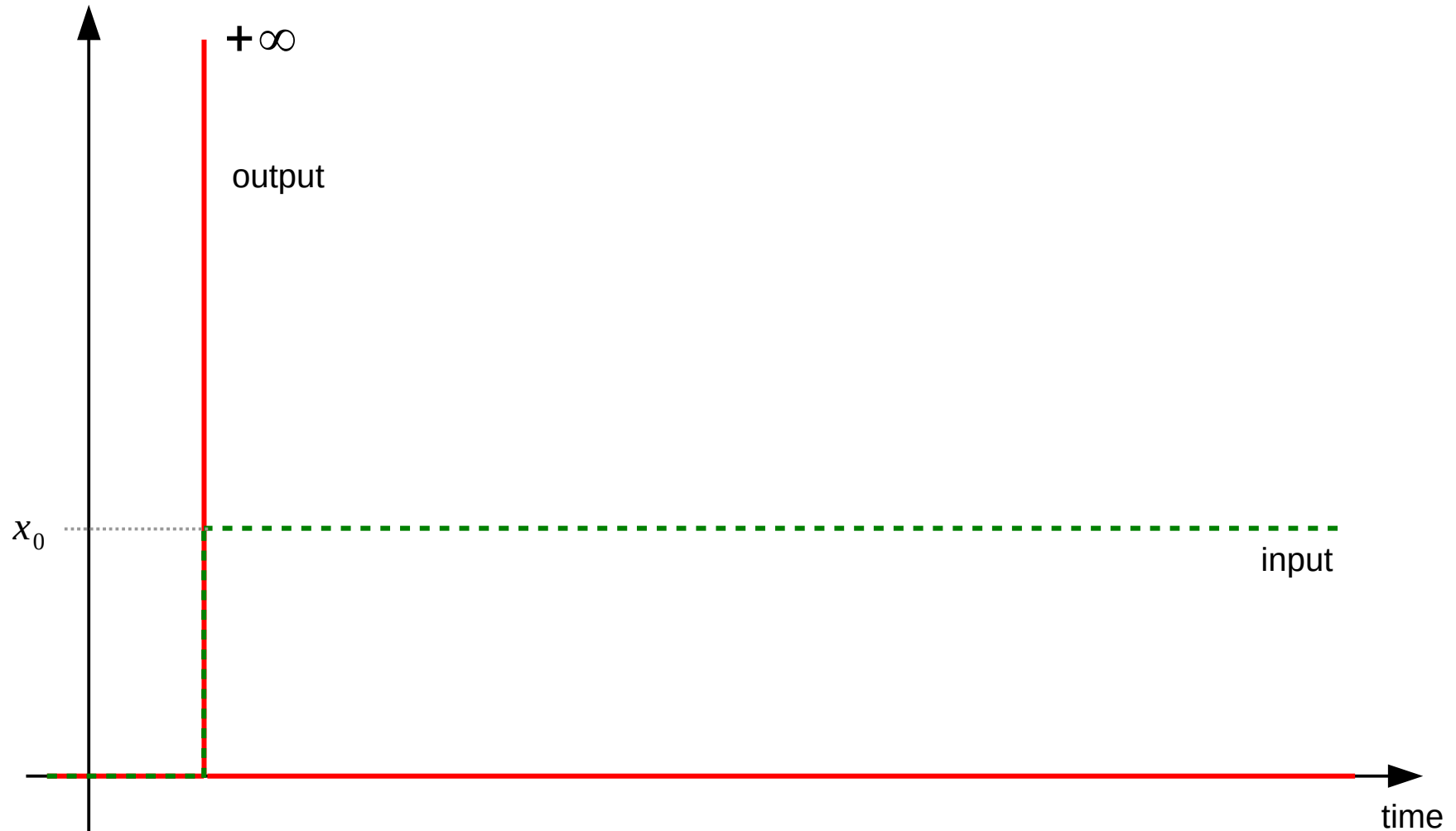
# PI - CONTROLLER

$$H(s) = K_p \left( 1 + \frac{1}{T_i s} \right)$$



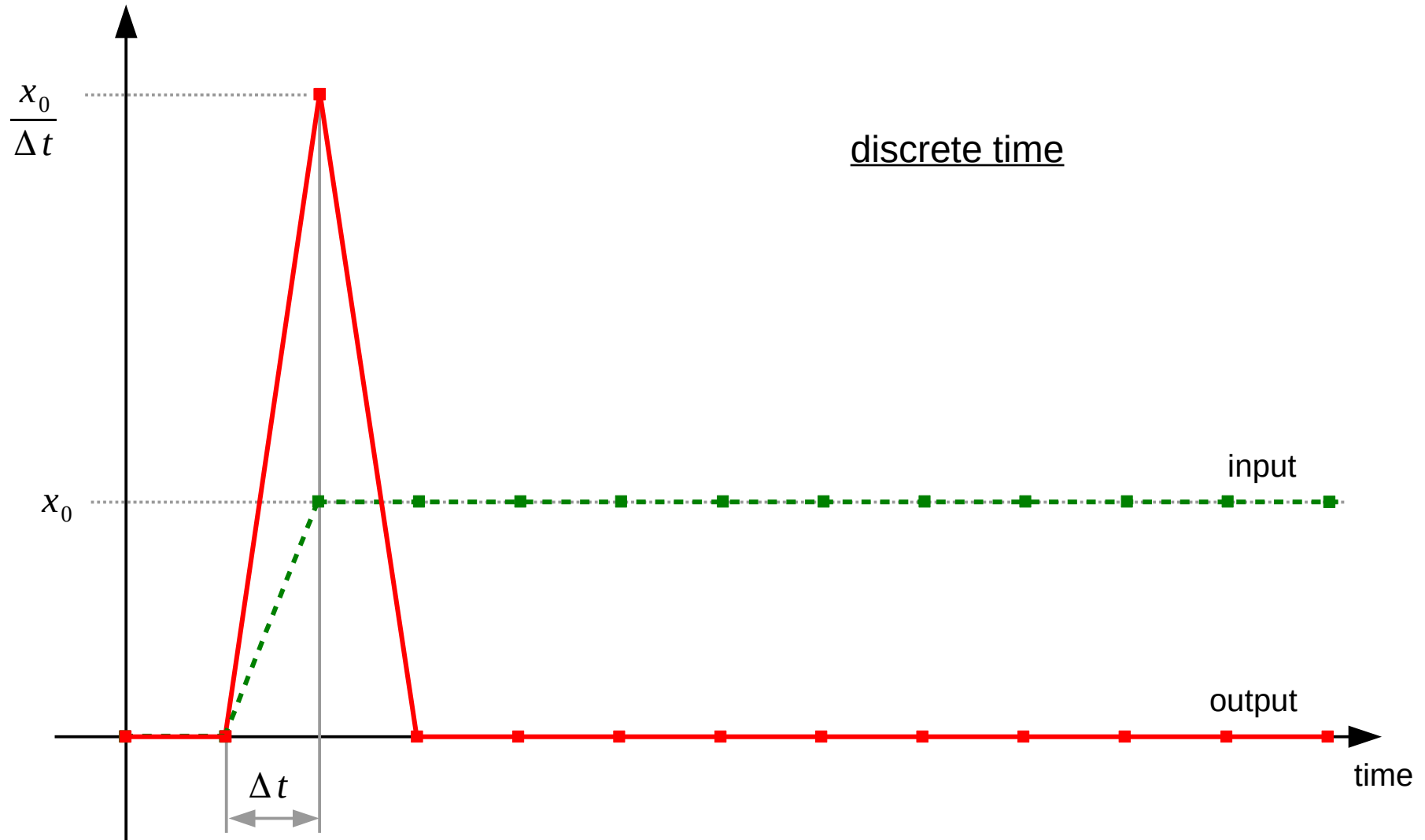
# D - CONTROLLER

$$H(s) = T_d s$$



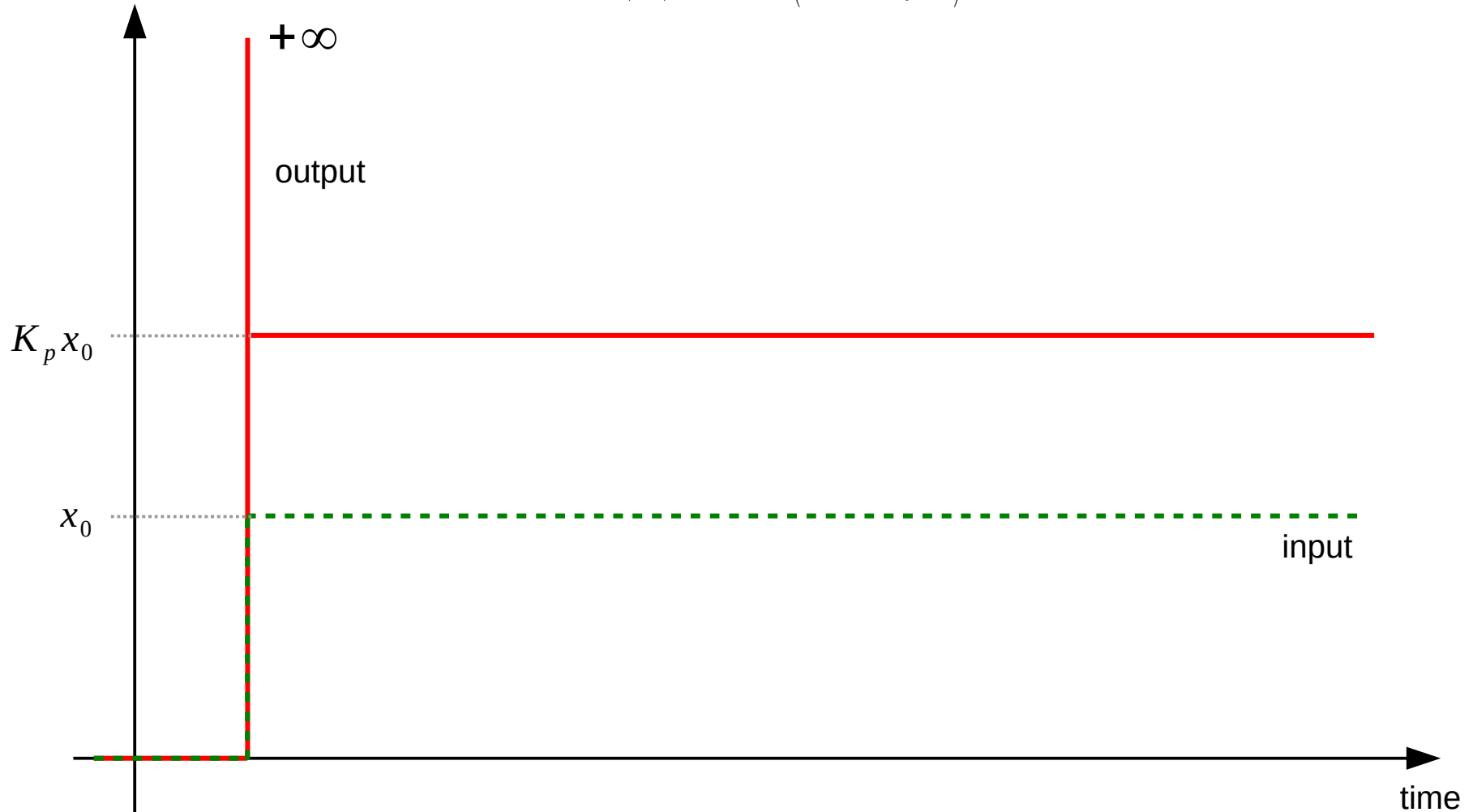
# D - CONTROLLER

$$H(s) = T_d s$$



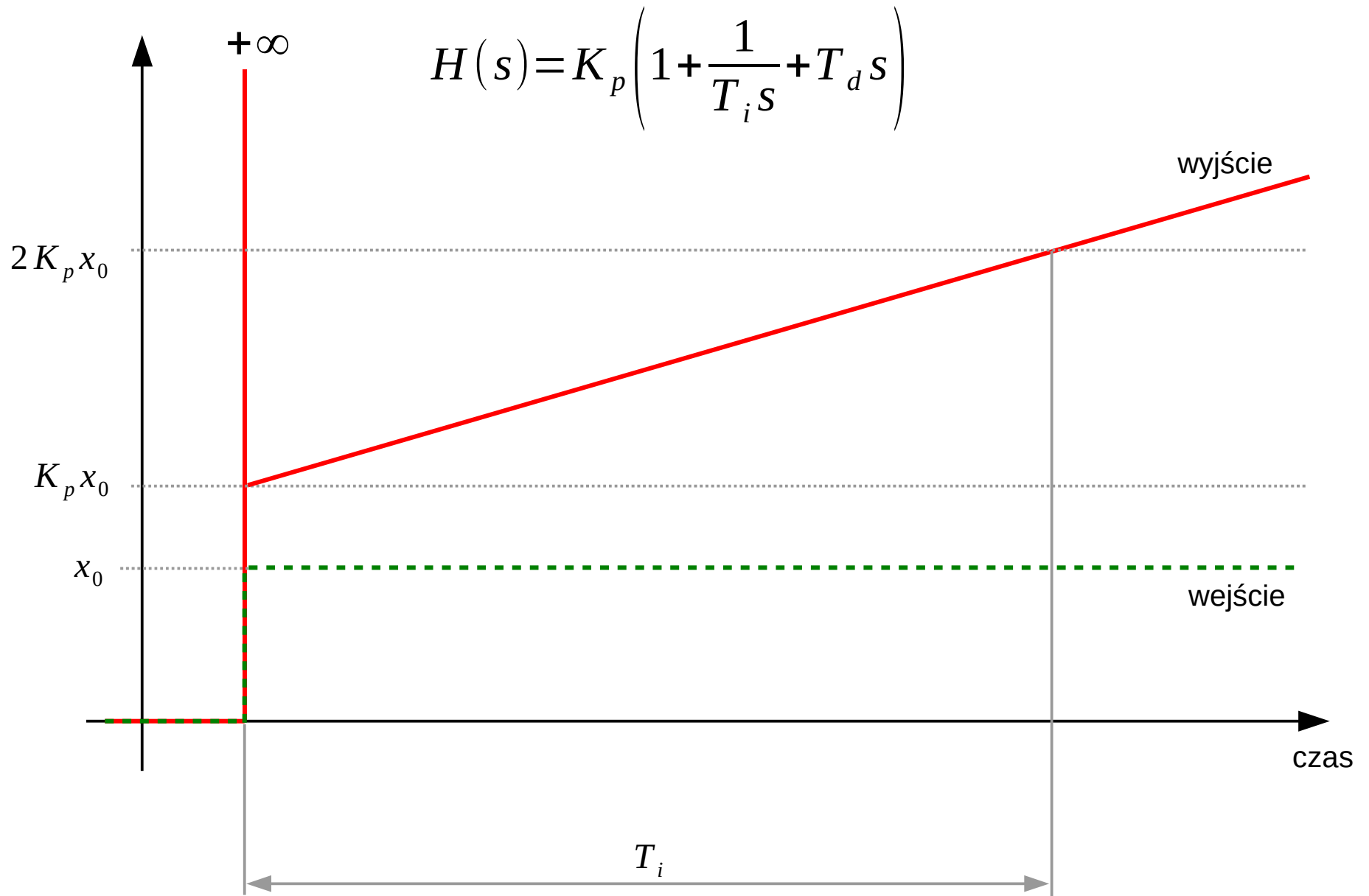
# PD - CONTROLLER

$$H(s) = K_P(1 + T_d s)$$



# PID – CONTROLLER

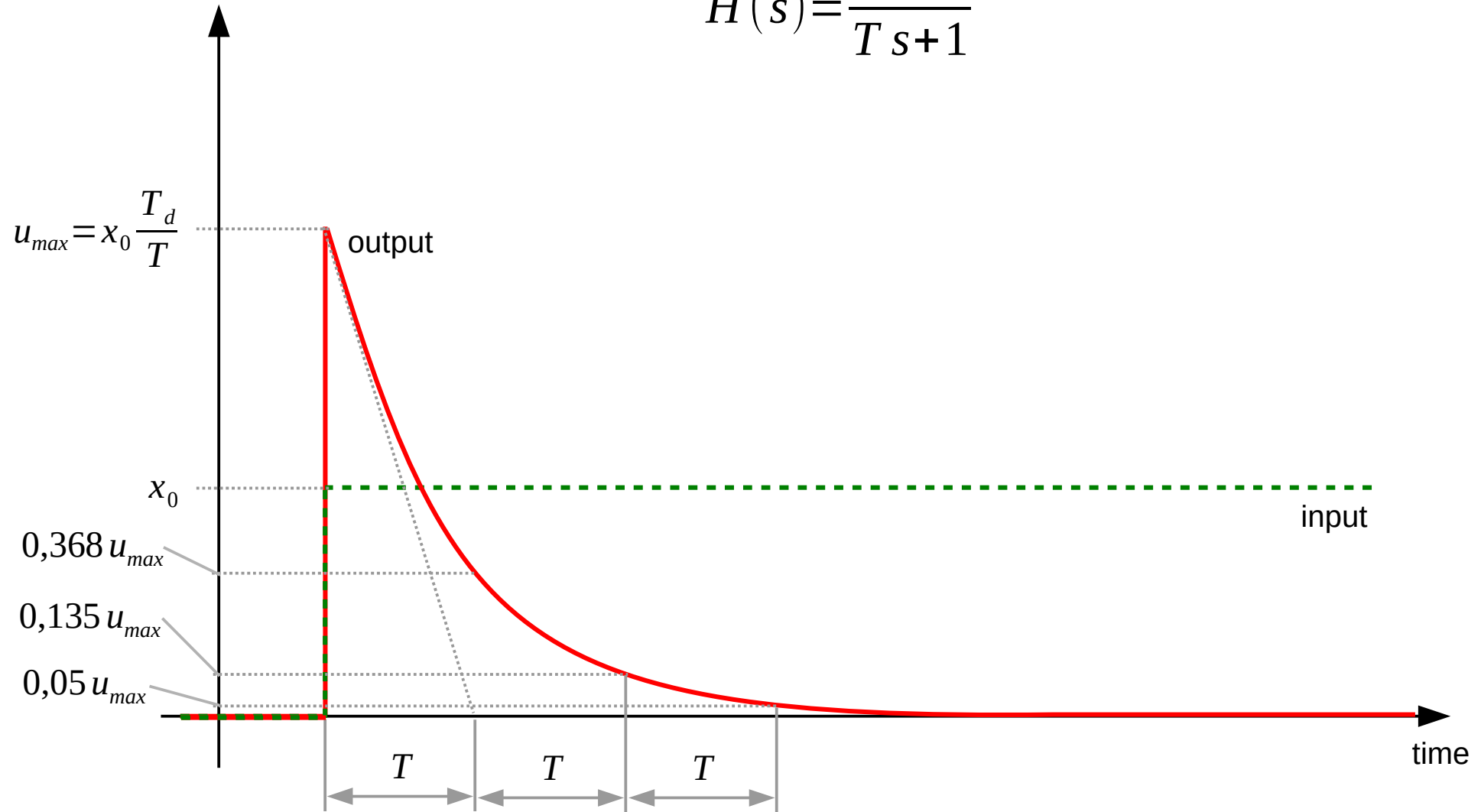
## standard form, ideal derivative





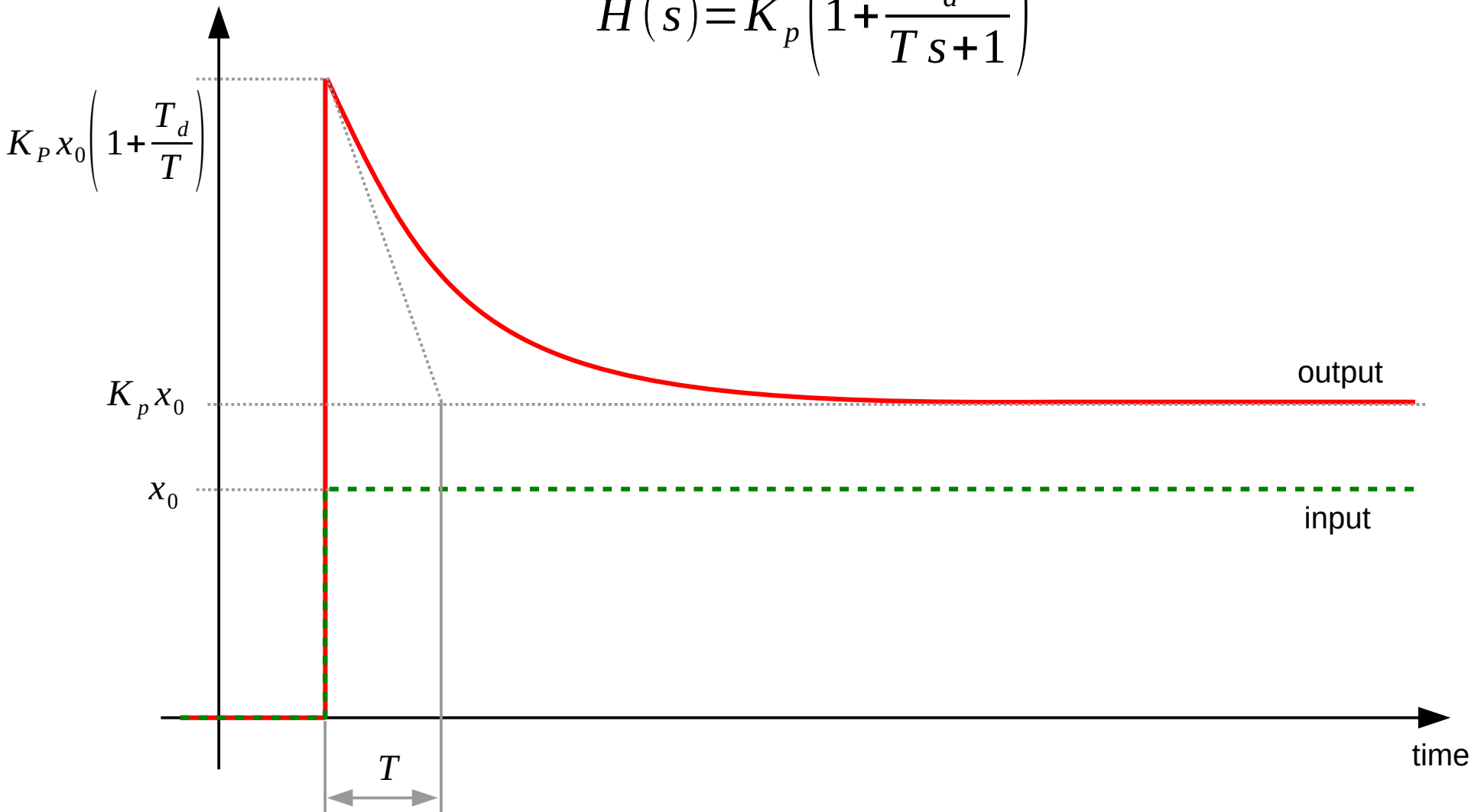
# D - CONTROLLER

$$H(s) = \frac{T_d s}{T s + 1}$$



# PD - CONTROLLER

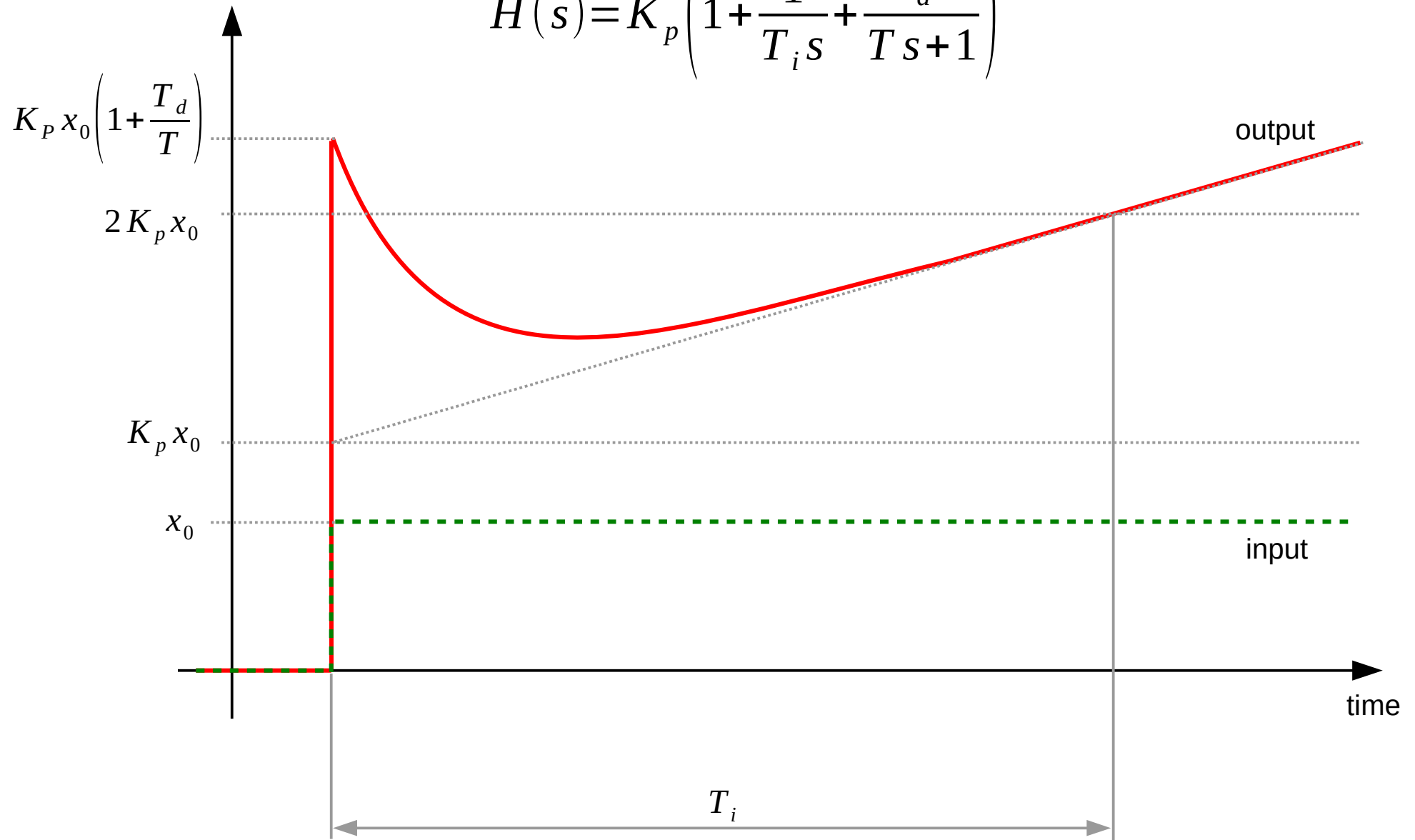
$$H(s) = K_p \left( 1 + \frac{T_d s}{T s + 1} \right)$$



# PID – CONTROLLER

## standard form, real derivative

$$H(s) = K_p \left( 1 + \frac{1}{T_i s} + \frac{T_d s}{T s + 1} \right)$$



# PID CONTROLLER

## important notes

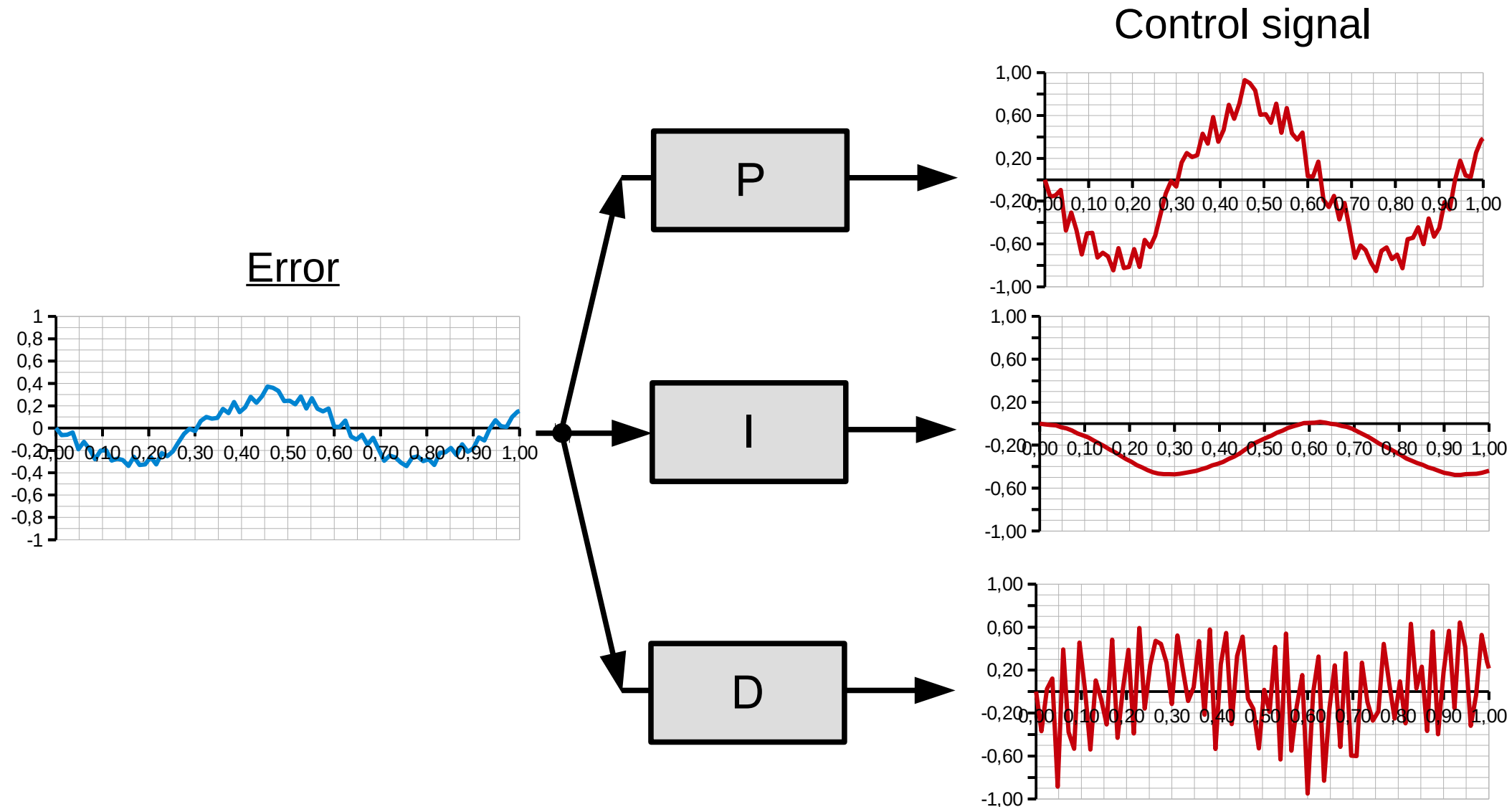
**Proportional term** – necessary part of the controller, creates a main part of control signal that bring output of the system closer to desired value; higher  $K_p$  coefficient gives lower errors; control signal is based on present error;

**Integral term** – this part of the controller accumulates error; for nonzero error control signal increases that helps to achieve zero error; control signal is based on past error values; “integral windup” problem;

**Derivative term** – this part of the controller reacts on error changes; for constant error control signal is zero; control signal is based on the trend of future error; this term is very sensitive to noise;

# PID CONTROLLER

## Influence of errors onto control signal



# PID CONTROLLER

## integral windup problem

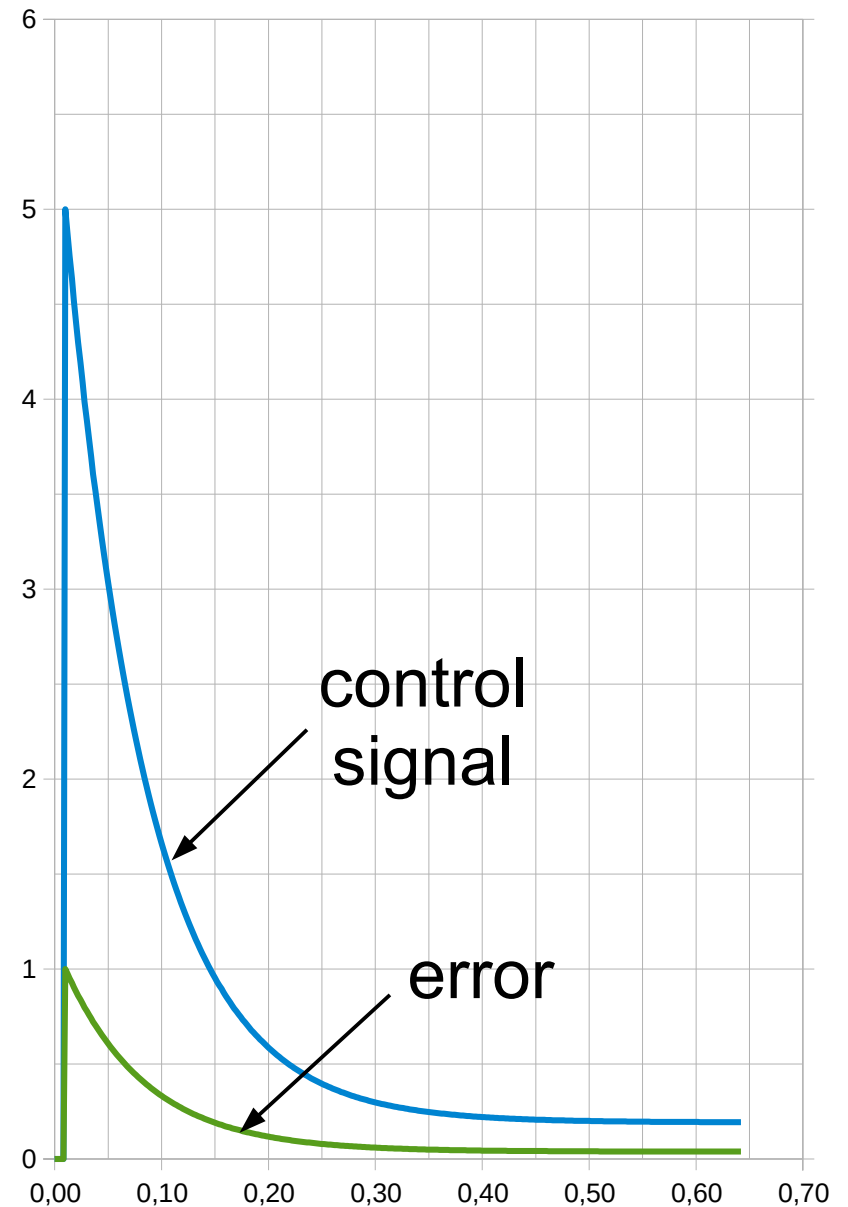
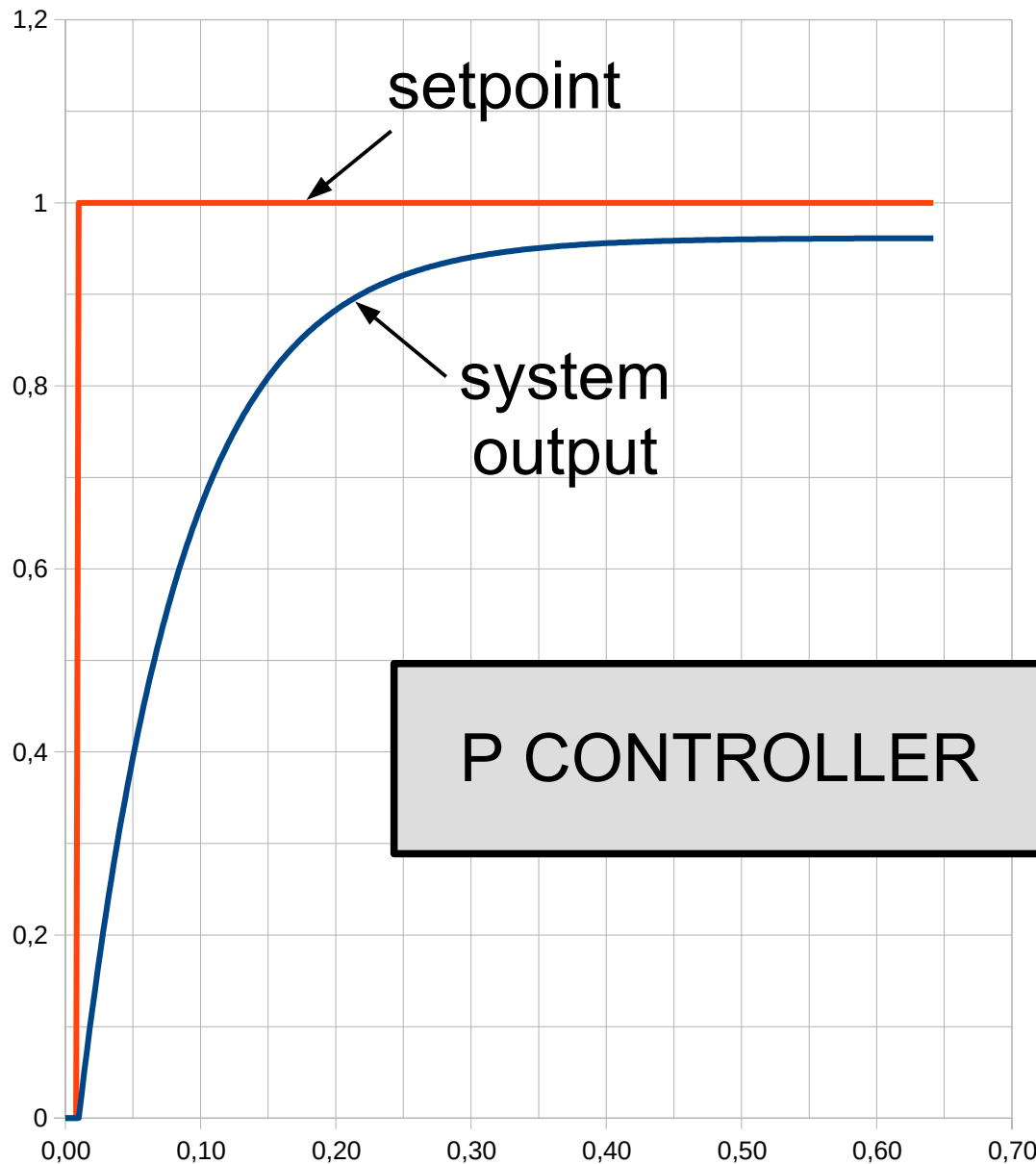
After a large change in a setpoint the integral term can produce very large control signal (higher than maximum possible) – system input is very height until accumulated error goes back close to zero.

Possible solution: disabling and zeroing integral term outside the small region around the setpoint.

*Additional reading: google: “integral anti-windup for pi controllers”*

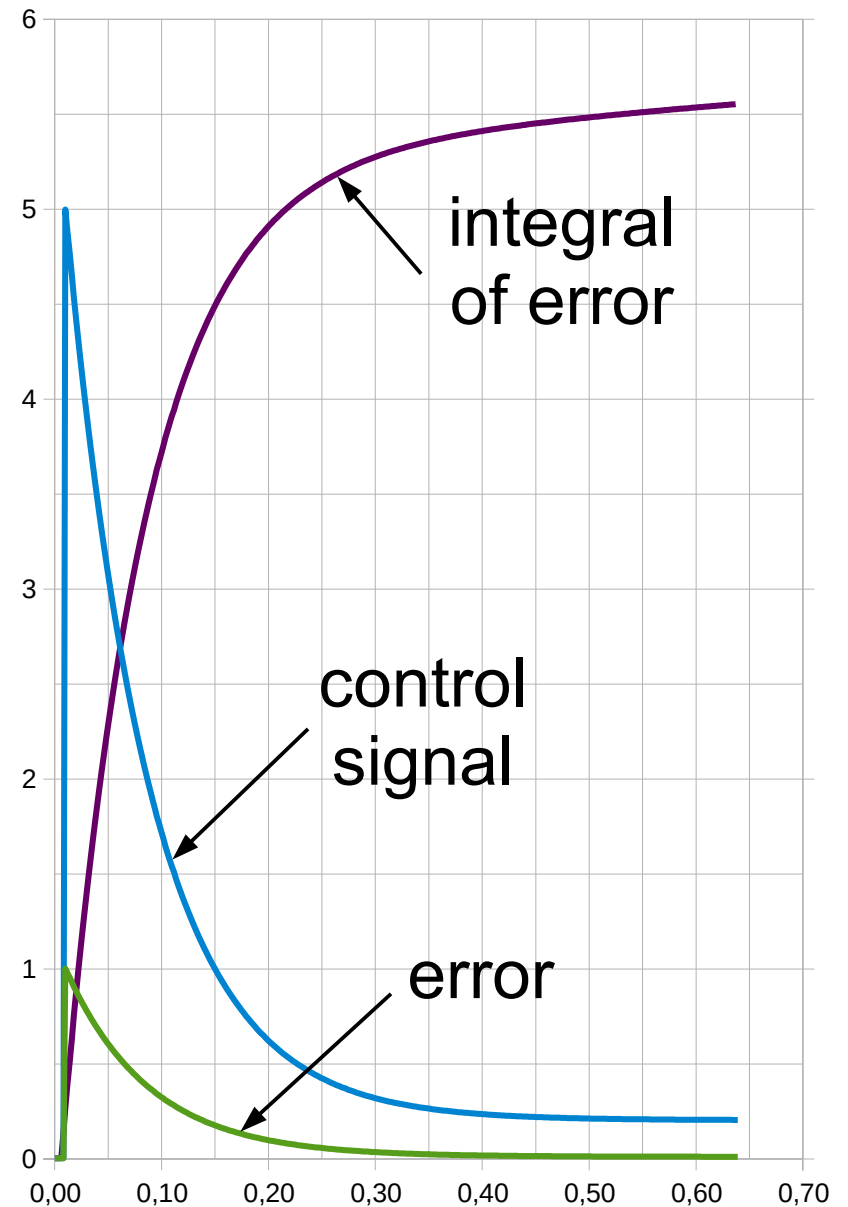
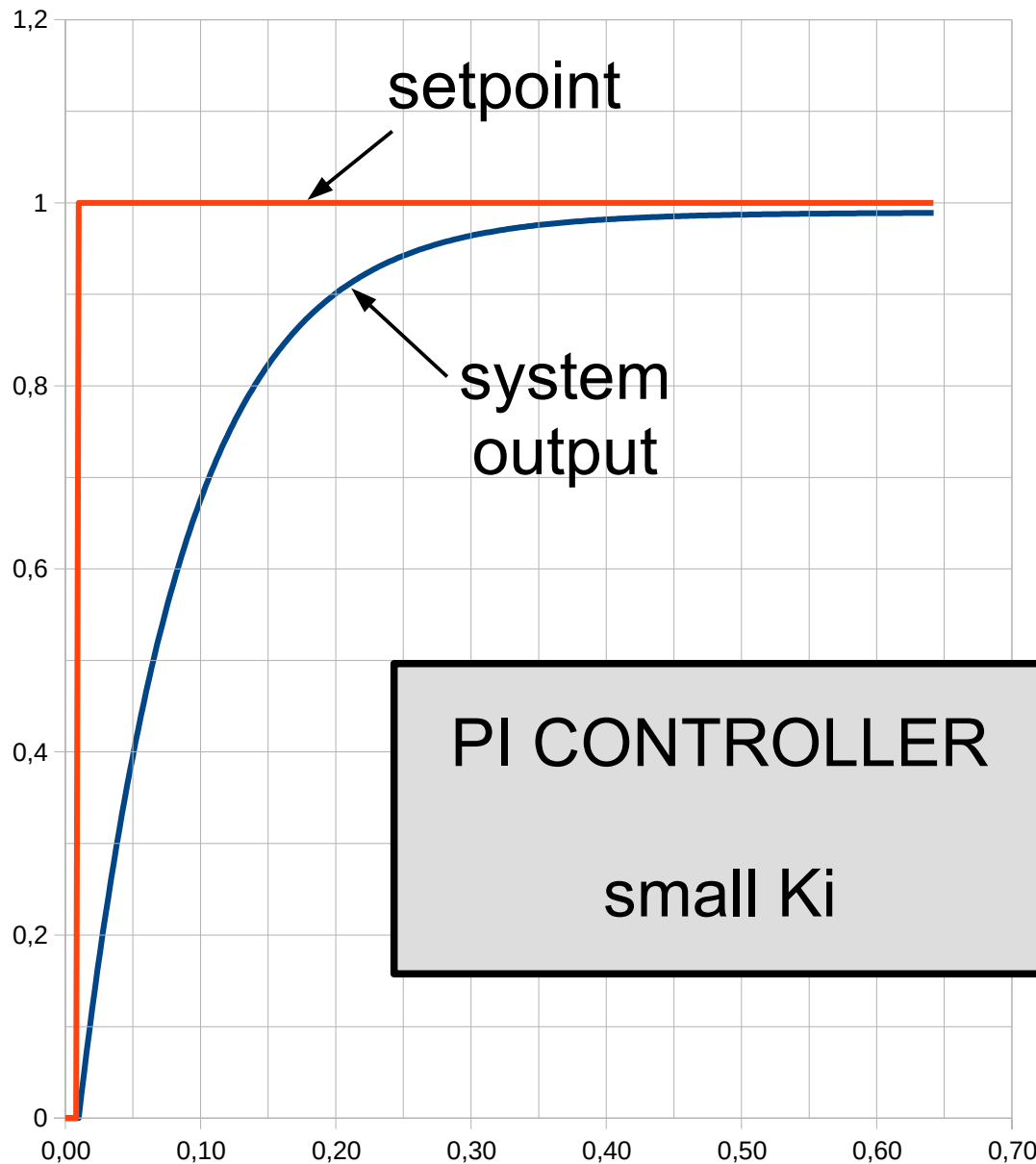
# PID CONTROLLER

integral windup problem example (1st order inertial system + parallel PID)



# PID CONTROLLER

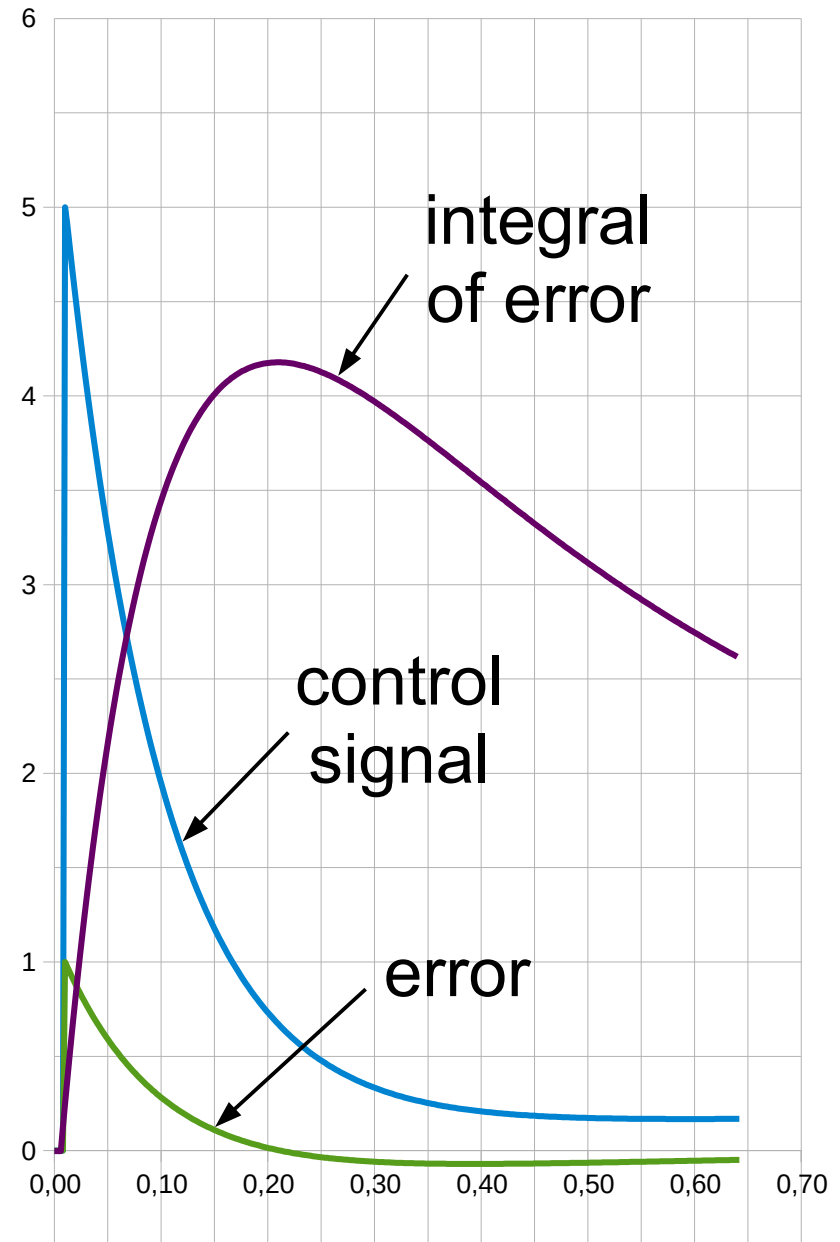
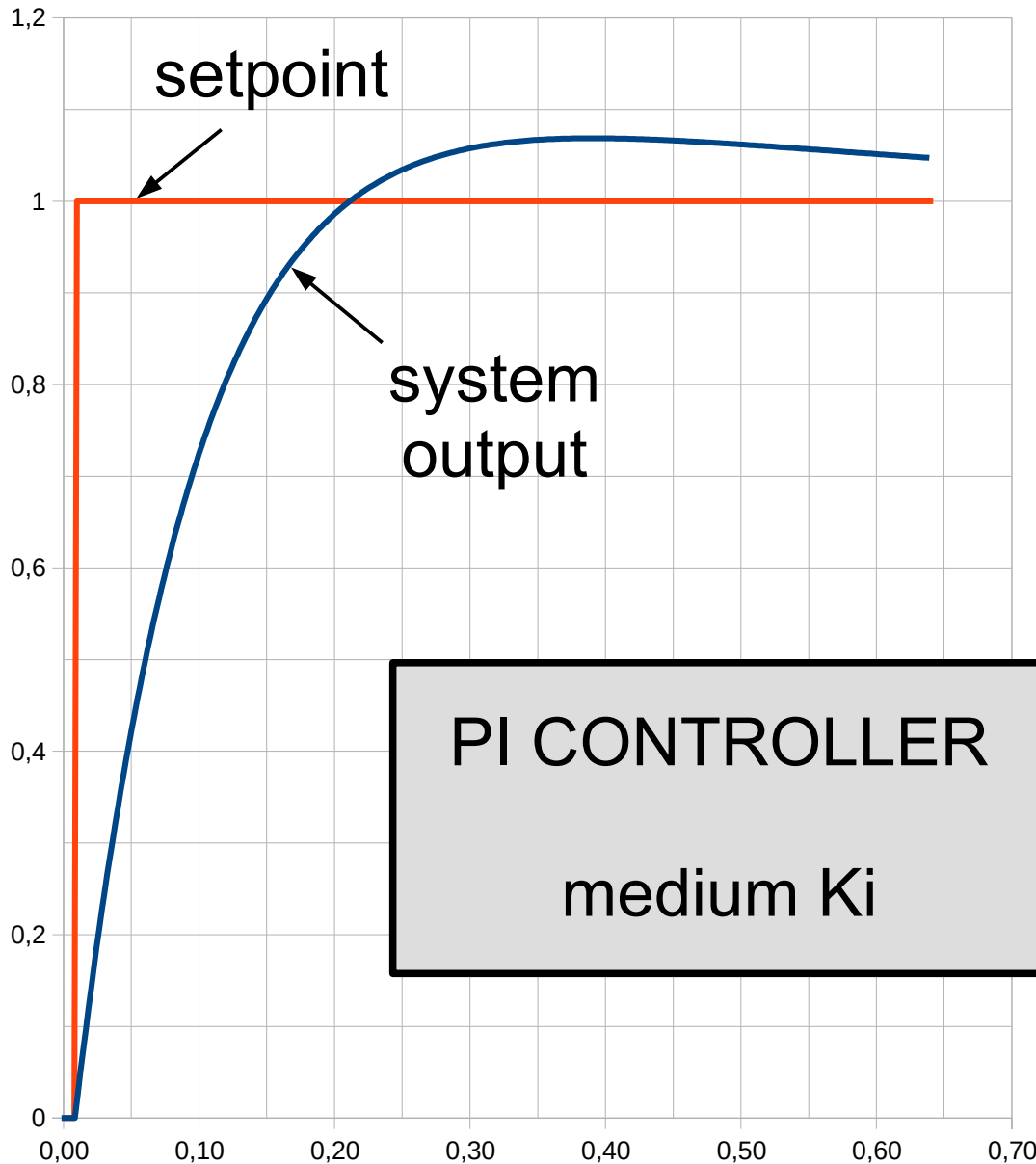
integral windup problem example (1st order inertial system + parallel PID)





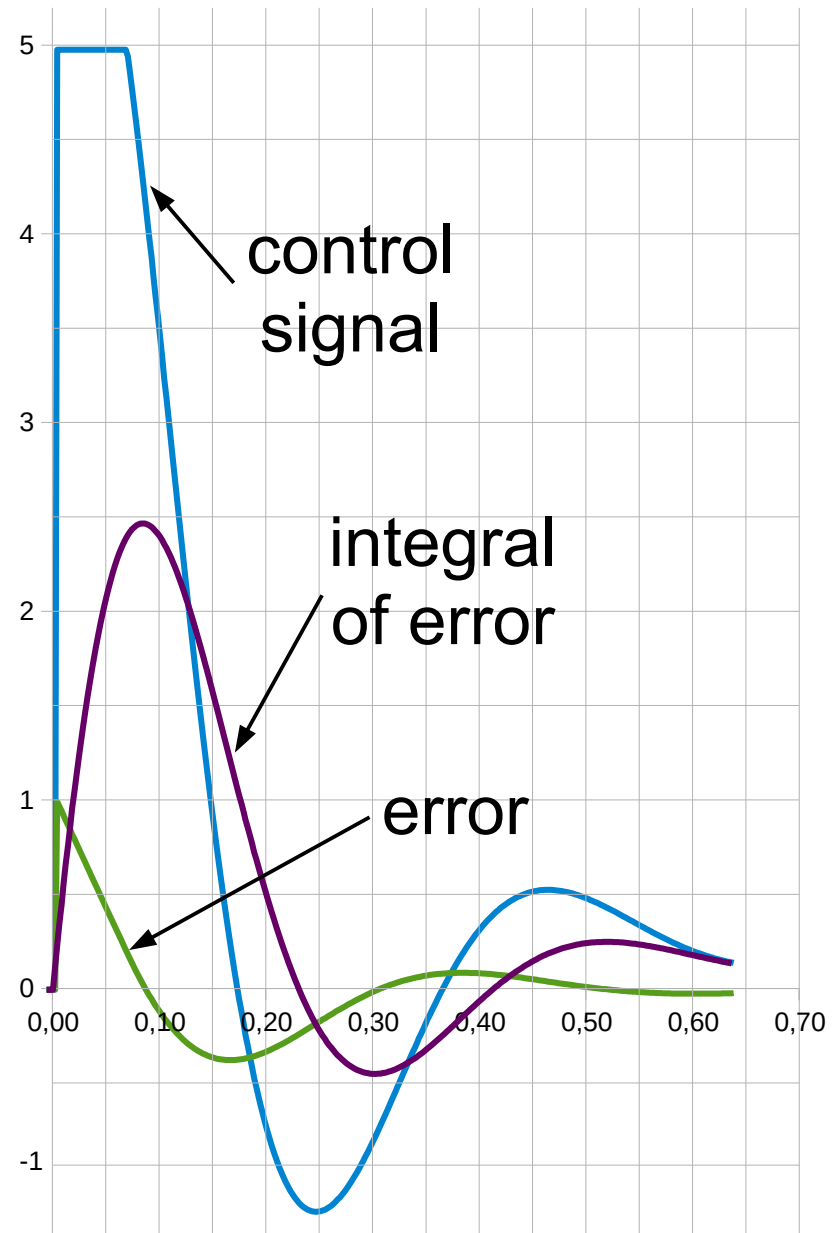
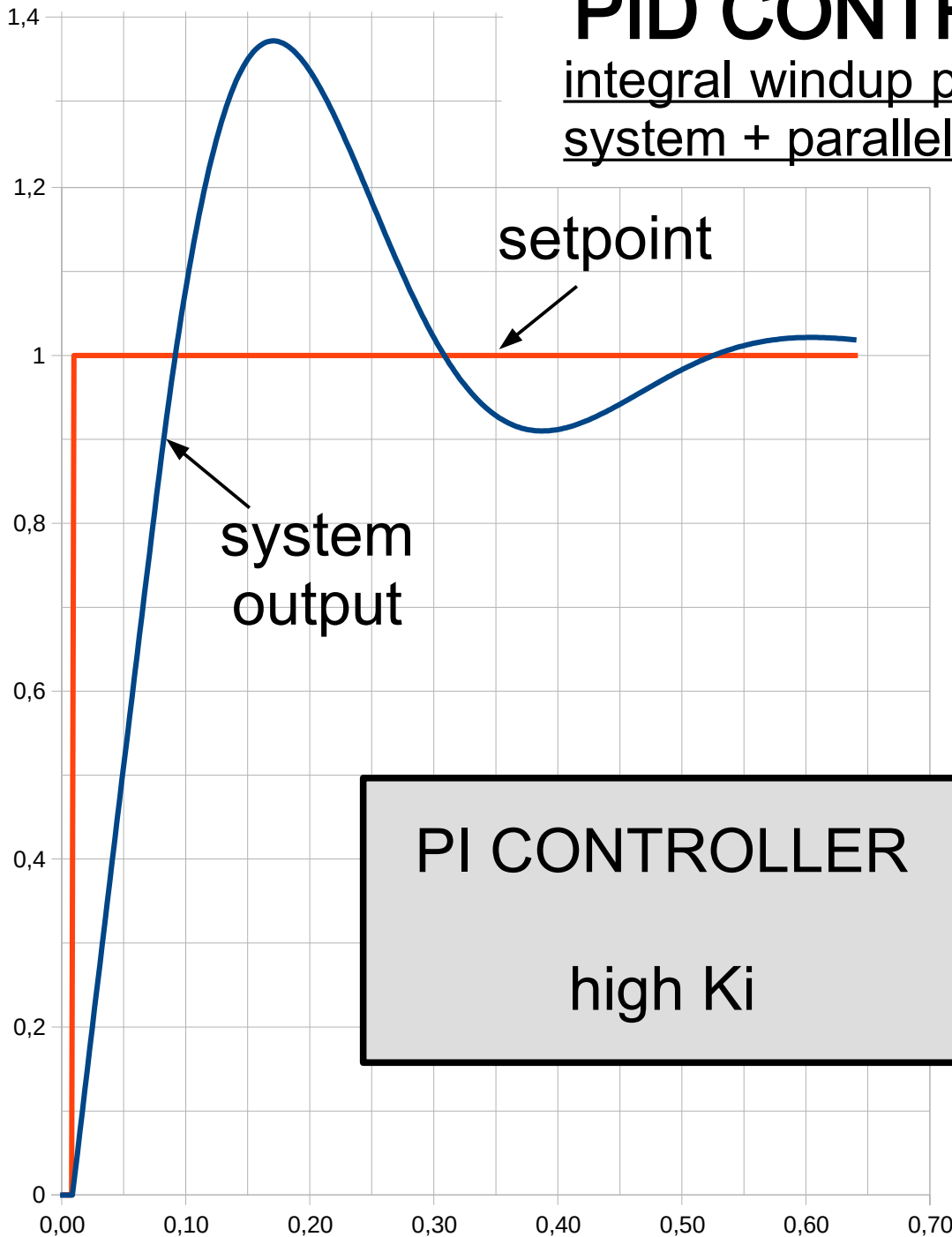
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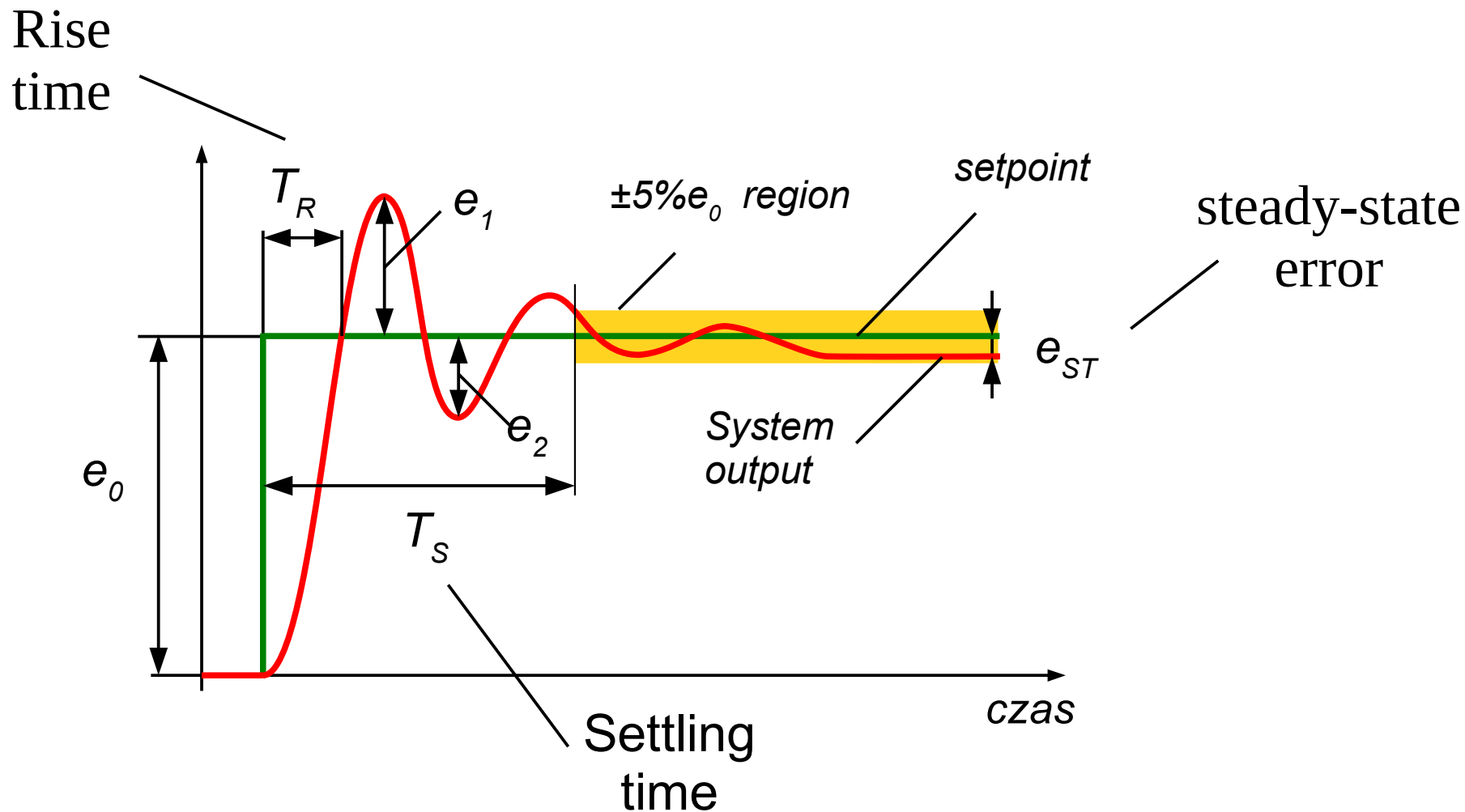


# PID CONTROLLER

integral windup problem example (1st order inertial system + parallel PID)



# Quality of the control process



Overshoot:  $w = \frac{e_1}{e_0} 100\%$

Damping:  $d = \frac{e_2}{e_1} 100\%$

# PID CONTROLLER

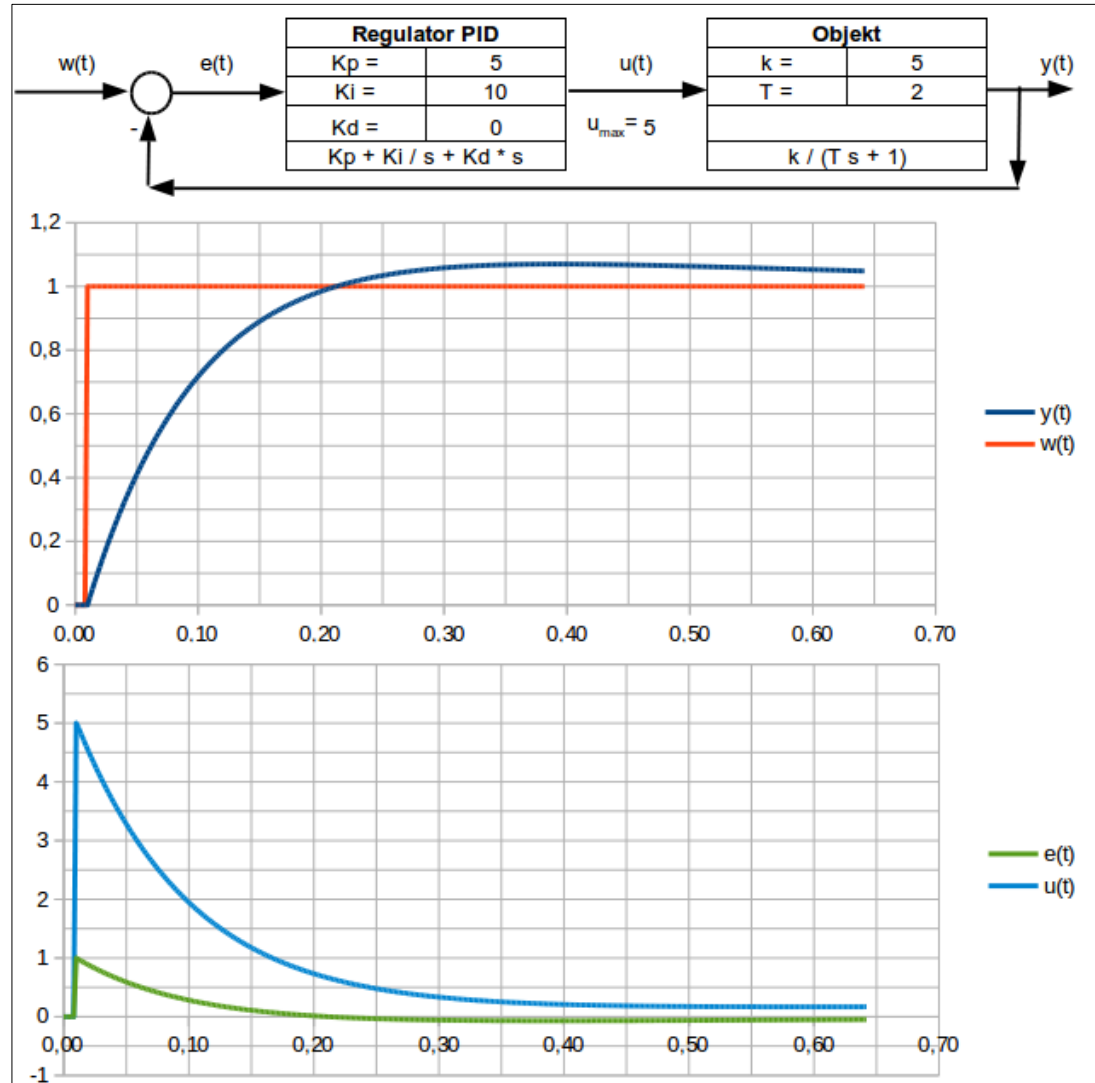
## tuning methods

Analytical	With a simulation	Experimental
<p>1<sup>st</sup> step: calculation of the system's reduced transfer function</p> <p>2<sup>nd</sup> step: calculation of the system's step response</p> <p>3<sup>rd</sup> step: tuning of the <math>K_p</math>, <math>K_i</math> and <math>K_d</math> coefficients to obtain desired shape of step response</p>	<p>1<sup>st</sup> step: calculation of the system's reduced transfer function</p> <p>2<sup>nd</sup> step: numerical implementation of the system's reduced transfer function</p> <p>3<sup>rd</sup> step: tuning of the <math>K_p</math>, <math>K_i</math> and <math>K_d</math> coefficients to obtain desired shape of the system's simulated outputs</p>	<p>Manual tuning</p> <p>or</p> <p>methods:</p> <ul style="list-style-type: none"><li>• Ziegler-Nichols<ul style="list-style-type: none"><li>• Pessen</li><li>• Cohen-Coon</li></ul></li><li>• Åström–Hägglund</li></ul>

# PID CONTROLLER

interactive simulation and tuning

*Download spreadsheet file from the website*



# PID CONTROLLER

## Ziegler-Nichols tuning method (PID in standard form)

1. Disable integral and derivative terms of the controller. Set proportional gain to small value.
2. Observe a step response of the output of control loop. Go to point 3, if you observe stable and consistent oscillations. If not, increase proportional gain and repeat step 2.

# PID CONTROLLER

## Ziegler-Nichols tuning method (PID in standard form)

1. Disable integral and derivative terms of the controller. Set proportional gain to small value.
2. Observe a step response of the output of control loop. Go to point 3, if you observe stable and consistent oscillations. If not, increase proportional gain and repeat step 2.
3. For the ultimate gain  $K_u$  from step 2 and oscillation period  $T_u$  calculate parameters of the controller according to the table:

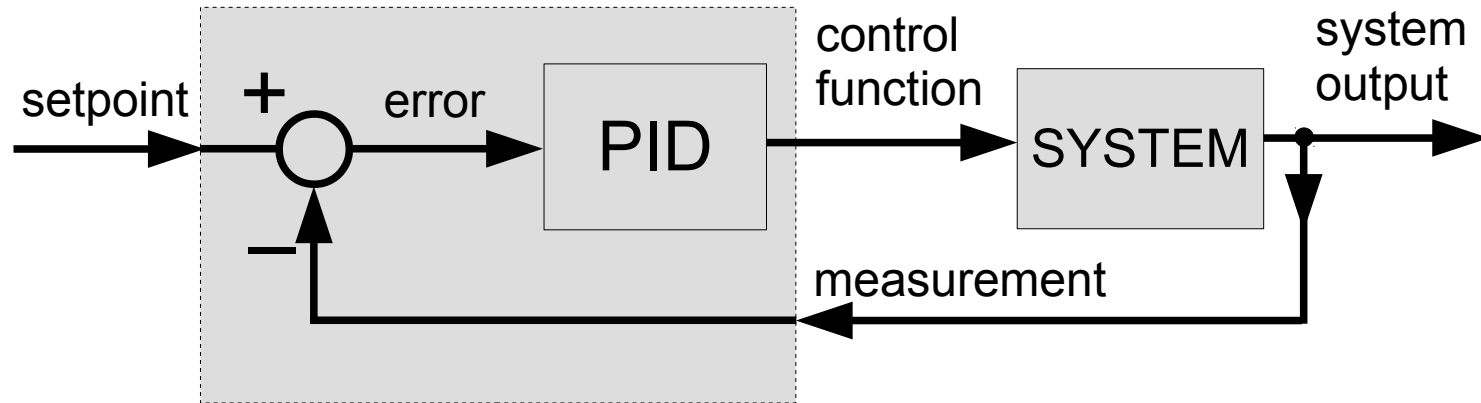
	$k_p$	$T_i$	$T_d$
Classic Ziegler-Nichols	$0.6 K_u$	$0.5 T_u$	$0.125 T_u$
Pessen	$0.7 K_u$	$0.4 T_u$	$0.15 T_u$
no overshoot	$0.2 K_u$	$0.5 T_u$	$0.333 T_u$

# PID CONTROLLER

programming

```
dt = 0.1
p_error = 0.
sum = 0.
Kp = 2.
Ki = 0.5
Kd = 0.01
start:
```

```
    setpoint = ...
    measurement = ...
    error = setpoint - measurement
    sum = sum + error * dt
    derivative = (error - p_error) / dt
    output = Kp*error + Ki*sum + Kd*derivative
    p_error = error
    wait(dt)
    goto start
```

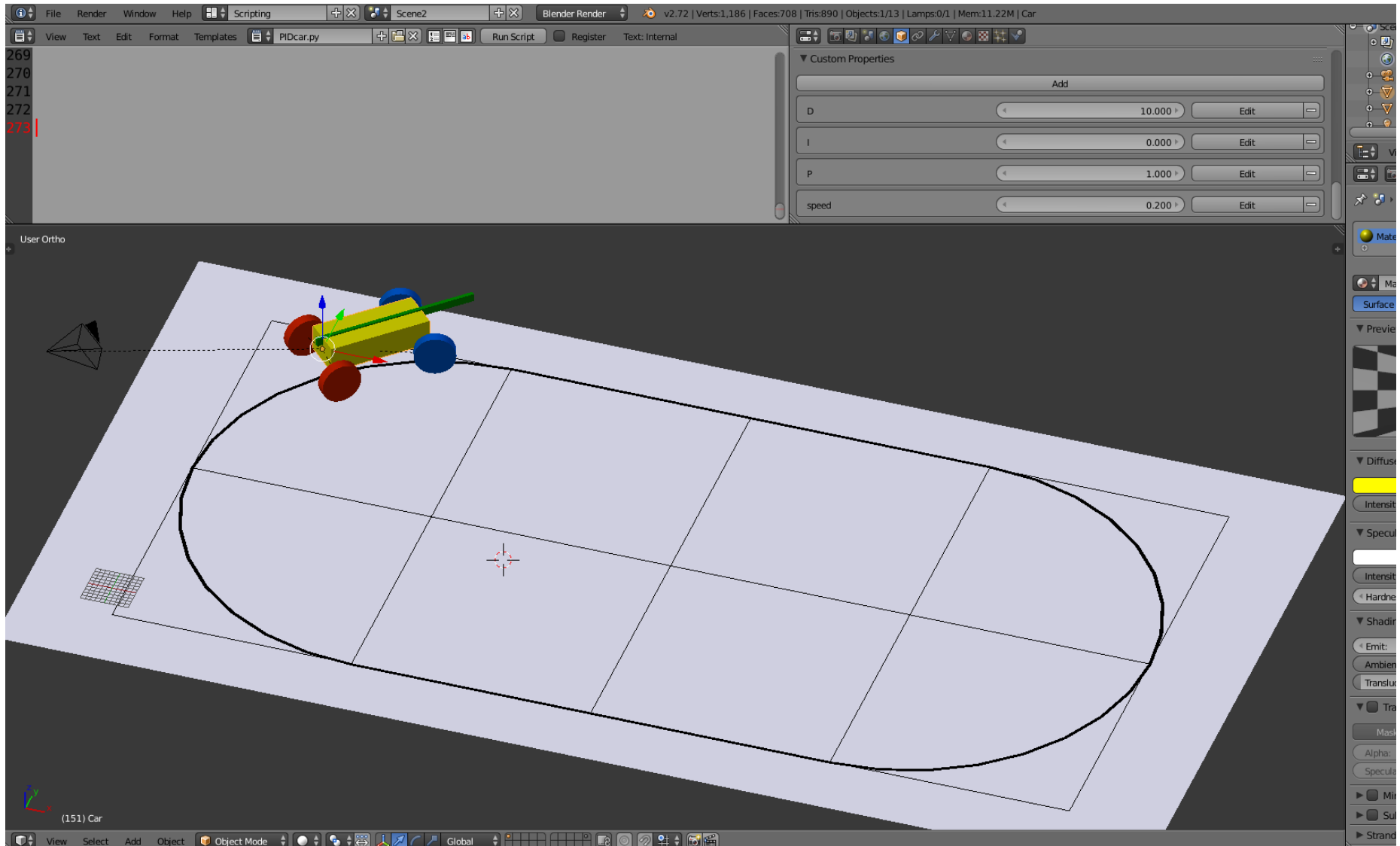




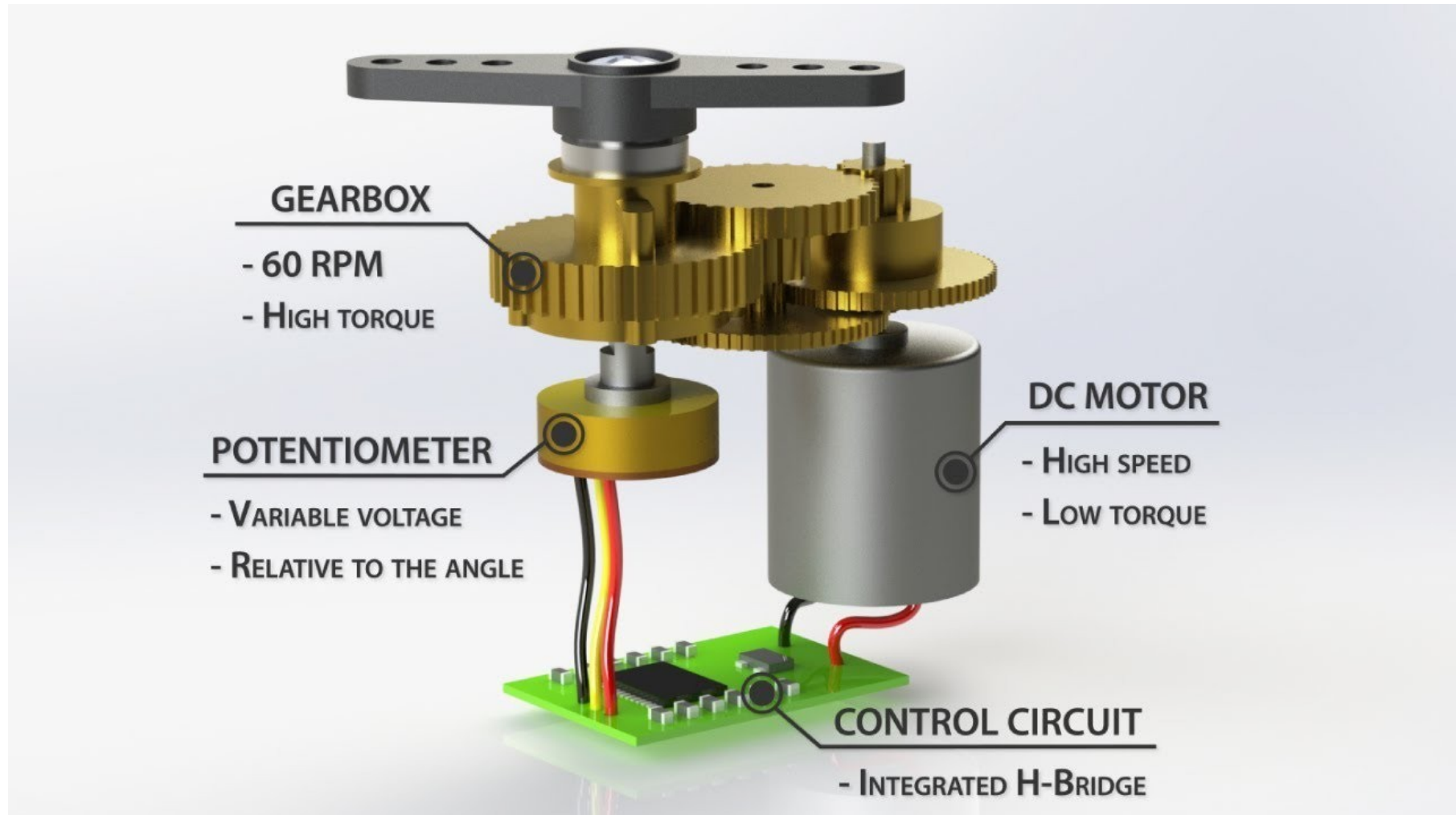
# PID CONTROLLER

interactive simulation

*PID for a car position control – real-time simulation*

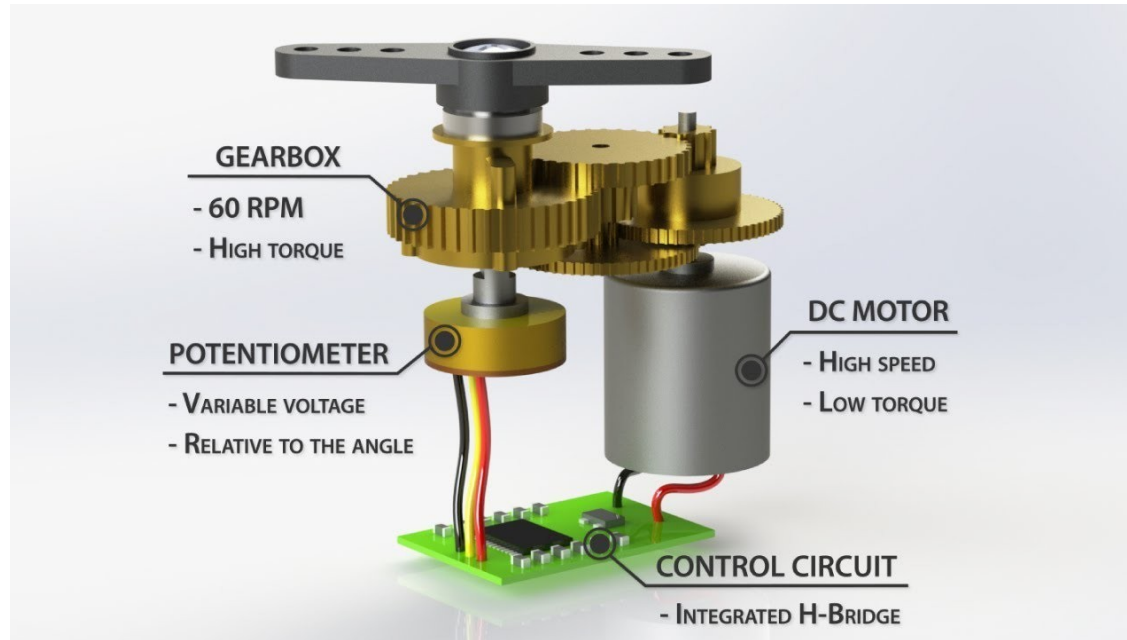


# Position control (servomotor)

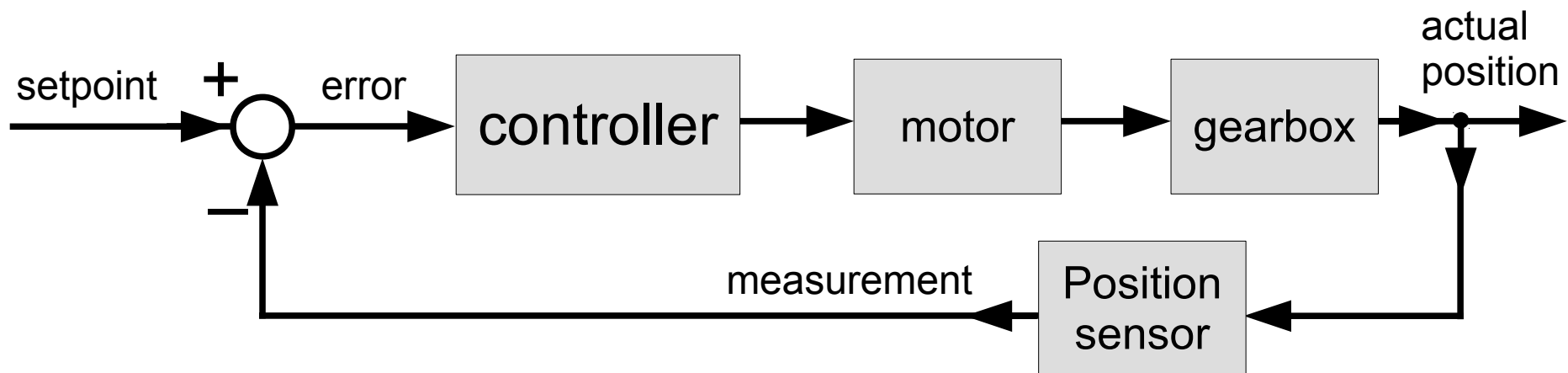


Source: <https://howtomechatronics.com/how-it-works/how-servo-motors-work-how-to-control-servos-using-arduino/>

# Position control (servomotor)



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# Stability

# Stability

## In mathematics:

- stability theory
- numerical stability
- stability in  
geometric theory

## In engineering:

- BIBO stability
- stability in flight  
dynamics
- ship stability

# Stability

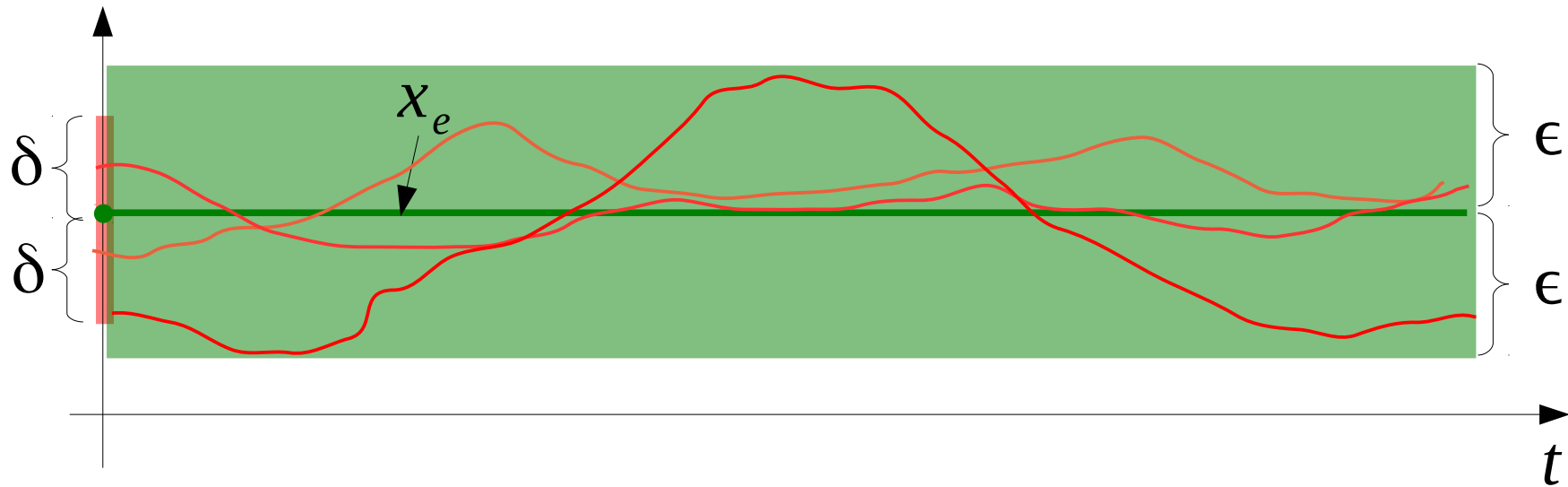
**Stability theory (math)** - study of the stability of differential equations' and dynamical systems' trajectories under small perturbations of initial conditions

- Lyapunov stability
- asymptotic stability
- orbital stability
- structural stability

# Lyapunov stability

$$\dot{x}(t) = f(x(t))$$

$$f(x_e) = 0, \quad x_e - \text{equilibrium}$$

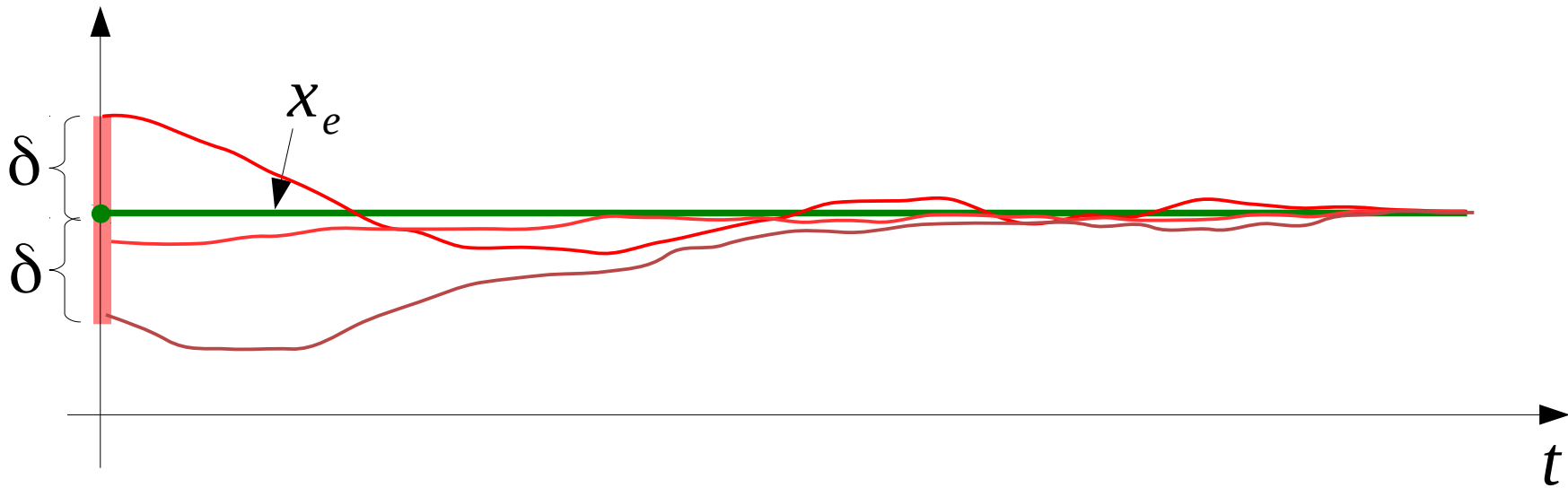


$$\forall_{t \geq 0} \quad \forall_{\epsilon > 0} \quad \exists_{\delta > 0} \quad \text{if } \|x(0) - x_e\| < \delta, \text{ then } \|x(t) - x_e\| < \epsilon$$

# Asymptotic stability

$$\dot{x}(t) = f(x(t))$$

$$f(x_e) = 0, \quad x_e - \text{equilibrium}$$



$$\forall_{t \geq 0} \quad \forall_{\epsilon > 0} \quad \exists_{\delta > 0} \quad \text{if } \|x(0) - x_e\| < \delta, \text{ then } \lim_{t \rightarrow \infty} \|x(t) - x_e\| = 0$$



# BIBO stability

## Bounded Input, Bounded Output stability (in signal processing and control theory)

a LTI SISO system is called BIBO stable if its output will stay bounded for any bounded input.

$x(t)$  - input

$y(t)$  - output

$$\exists_{0 < A < \infty} \exists_{0 < B < \infty} \forall_{t \geq 0} \text{ if } |x(t)| \leq A, \text{ then } |y(t)| \leq B$$

# STABILITY CRITERIA

**General stability criterion**

**Hurwitz criterion**

**Nyquist stability criterion**

# General stability criterion

# General stability criterion

$$H(s) = \frac{Y(s)}{X(s)} = \frac{1}{s - p_1}$$

$p_1$  - pole of transfer function

input:  $x(t) = \delta(t)$ ,  $X(s) = L^{-1}\{\delta(t)\} = 1$

impulse response:  $y(t) = L^{-1}\{x(s)H(s)\} = L^{-1}\left\{1 \frac{1}{s - p_1}\right\} = e^{p_1 t}$

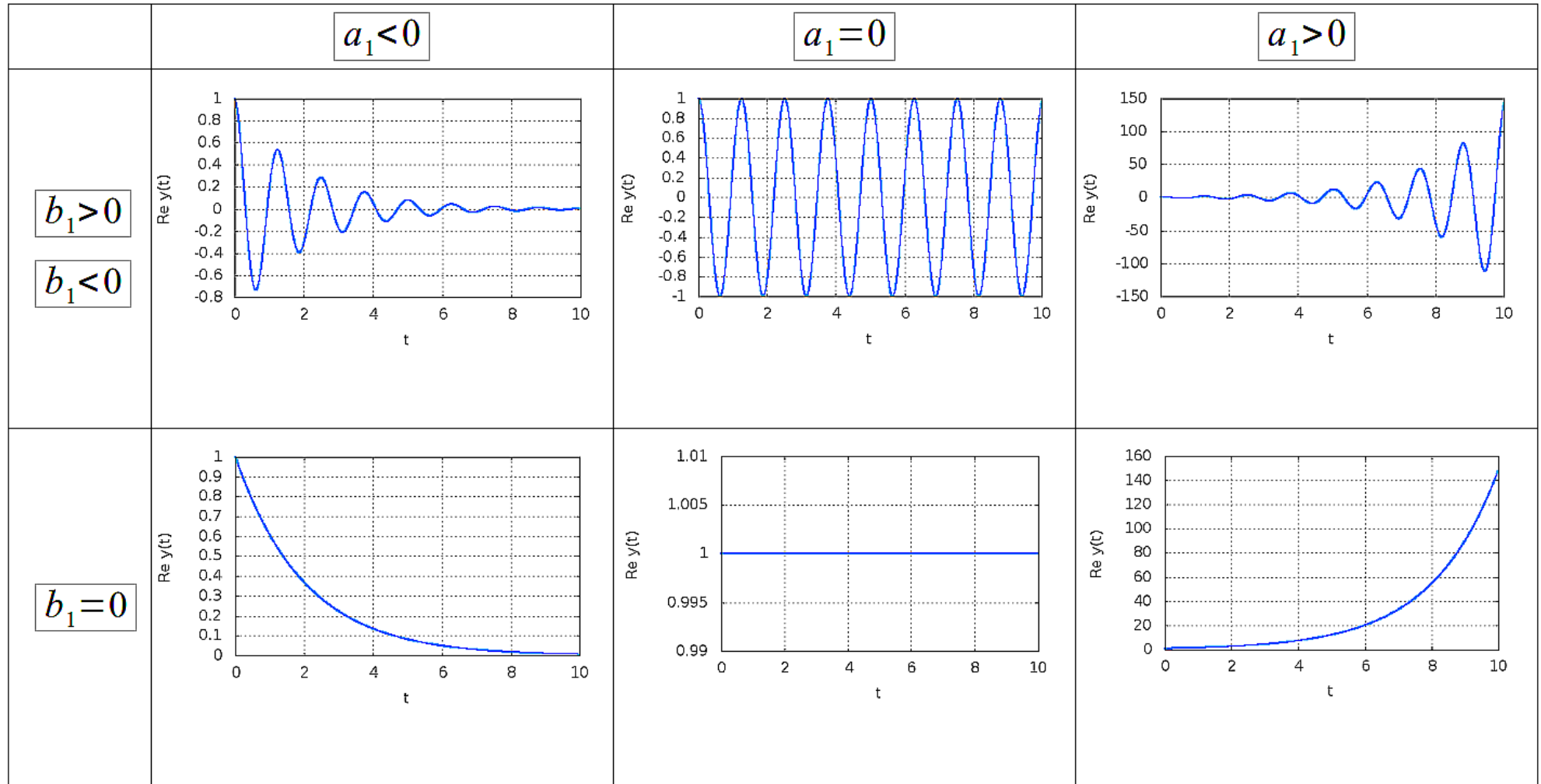
$$y(t) = e^{(a_1 + j b_1)t} = e^{a_1 t} e^{j b_1 t} = e^{a_1 t} (\cos b_1 t + j \sin b_1 t)$$

$$\text{Re } y(t) = e^{a_1 t} \cos b_1 t$$

$$H(s) = \frac{Y(s)}{X(s)} = \frac{1}{s - p_1}$$

$$\text{Re } y(t) = e^{a_1 t} \cos b_1 t$$

$$\begin{aligned} \text{Re}(p_1) &= a_1 \\ \text{Im}(p_1) &= b_1 \end{aligned}$$

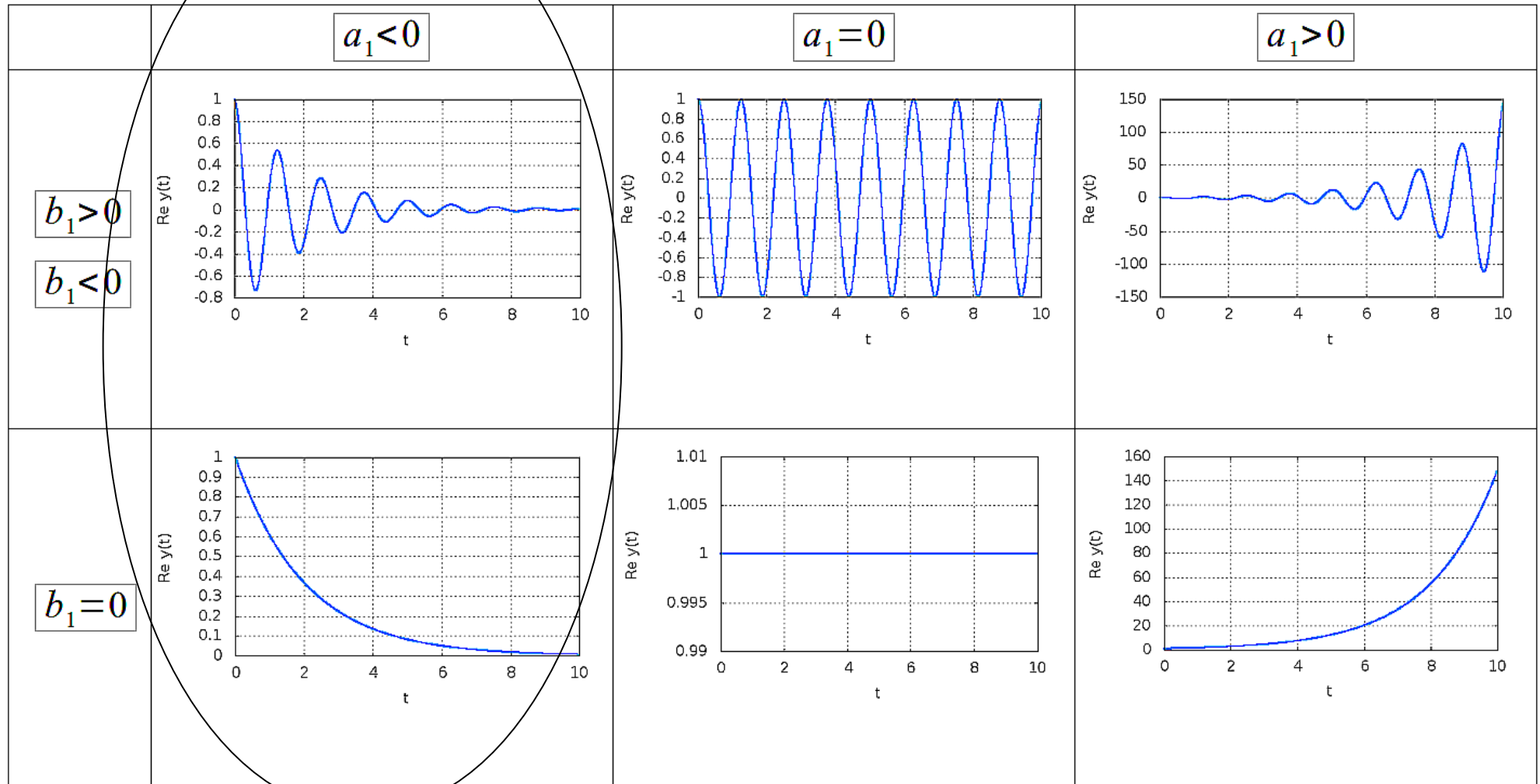


$$H(s) = \frac{Y(s)}{X(s)} = \frac{1}{s - p_1}$$

$$\operatorname{Re} y(t) = e^{a_1 t} \cos b_1 t$$

$$\operatorname{Re}(p_1) = a_1$$

$$\operatorname{Im}(p_1) = b_1$$



$H(s)$  asymptotically stable, if  $\operatorname{Re}(p_1) < 0$

# General stability criterion (definition)

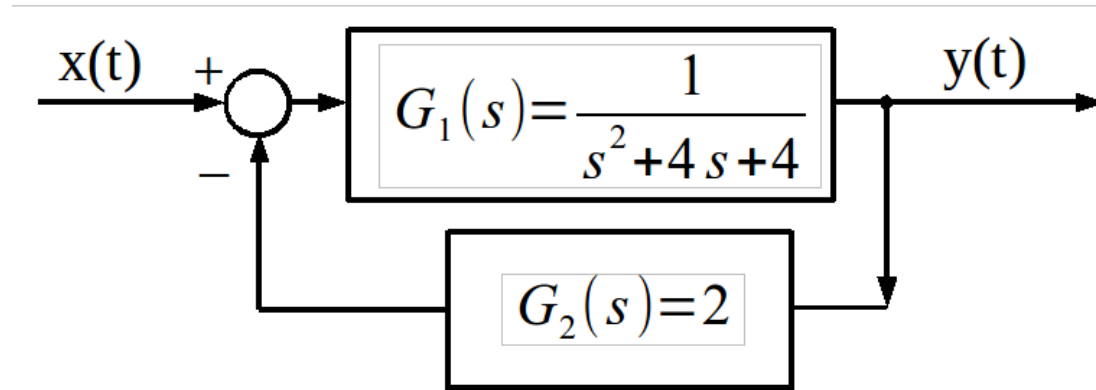
LTI SISO system is stable, if real parts of all transfer function's poles are less than zero.

$$H(s) = \frac{(s - z_1)(s - z_2) \dots (s - z_m)}{(s - p_1)(s - p_2) \dots (s - p_n)}$$

$H(s)$  is stable if:  $\text{Re } p_1 < 0 \wedge \text{Re } p_2 < 0 \wedge \dots \wedge \text{Re } p_n < 0$

# Example 1

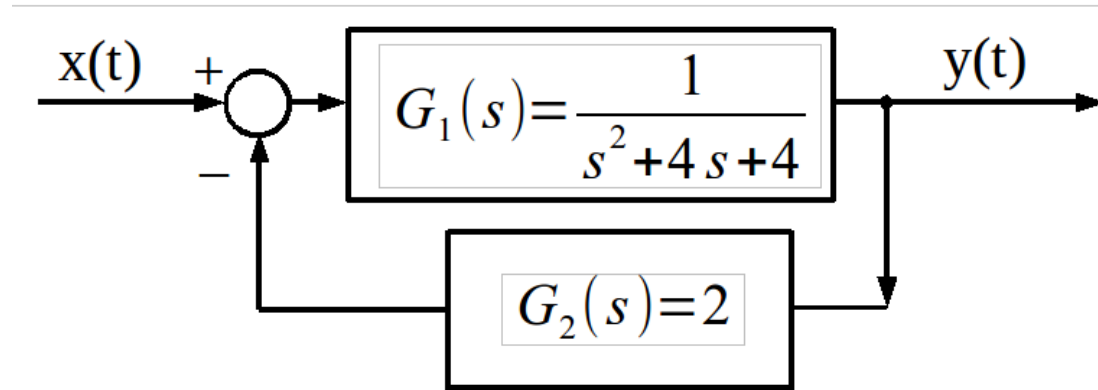
Check stability of the presented system using the general stability criterion.





# Example 1

Check stability of the presented system using the general stability criterion



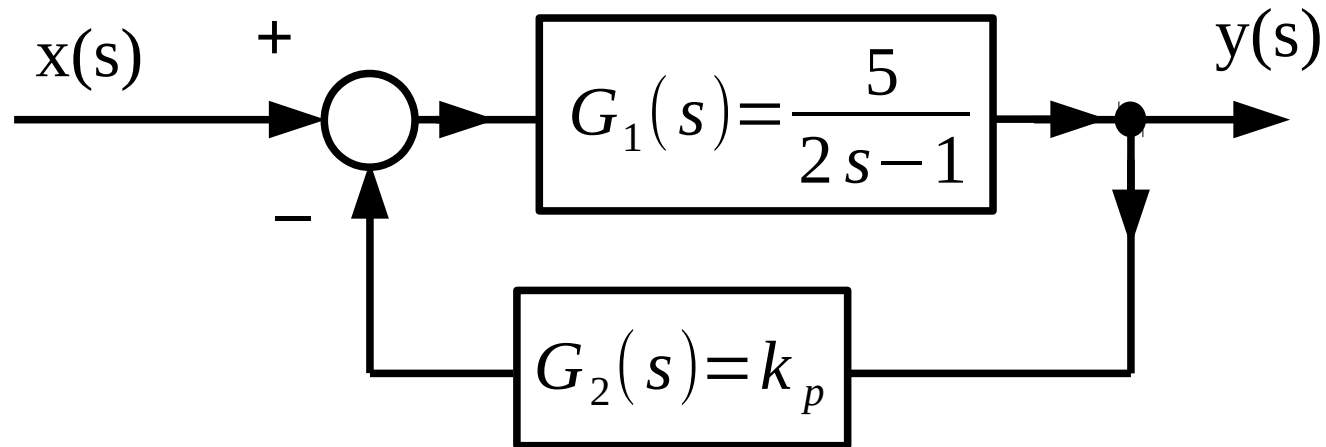
$$G(s) = \frac{Y(s)}{X(s)} = \frac{G_1}{1 + G_1 G_2} = \frac{1}{s^2 + 4s + 6} = \frac{1}{(s - s_1)(s - s_2)}$$

$$s_1 = -2 - 2\sqrt{2}j, \quad s_2 = -2 + \sqrt{2}j$$

$\Re(s_1) < 0 \wedge \Re(s_2) < 0 \Rightarrow$  system is stable from general stability criterion

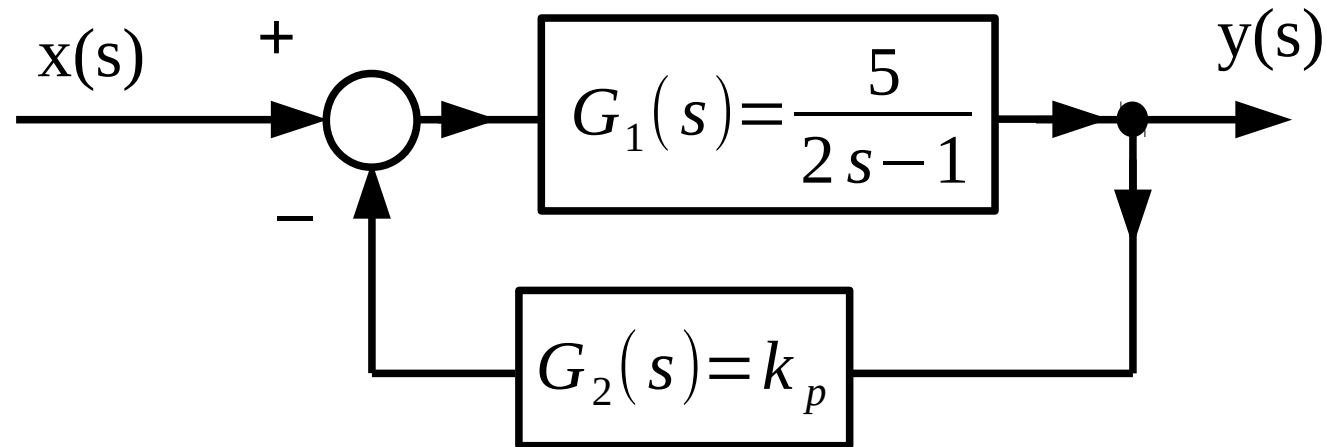
## Example 2

Choose values of  $K_p$  to obtain system stability using the general stability criterion



## Example 2

Choose values of  $K_p$  to obtain system stability using the general stability criterion



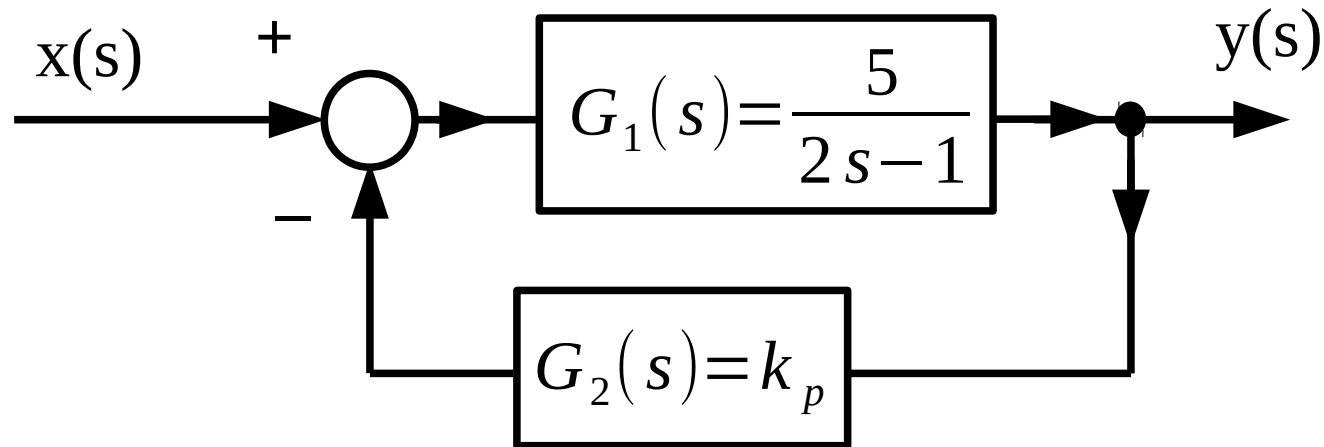
$$G(s) = \frac{Y(s)}{X(s)} = \frac{G_1}{1 + G_1 G_2} = \frac{5}{2} \frac{1}{s - \left( \frac{1}{2} - \frac{5}{2} k_p \right)}$$

$$p_1 = \left( \frac{1}{2} - \frac{5}{2} k_p \right)$$

System is stable, if  $\Re(p_1) < 0 \Rightarrow k_p > \frac{1}{5}$

## Example 2

Choose values of  $K_p$  to obtain system stability using the general stability criterion

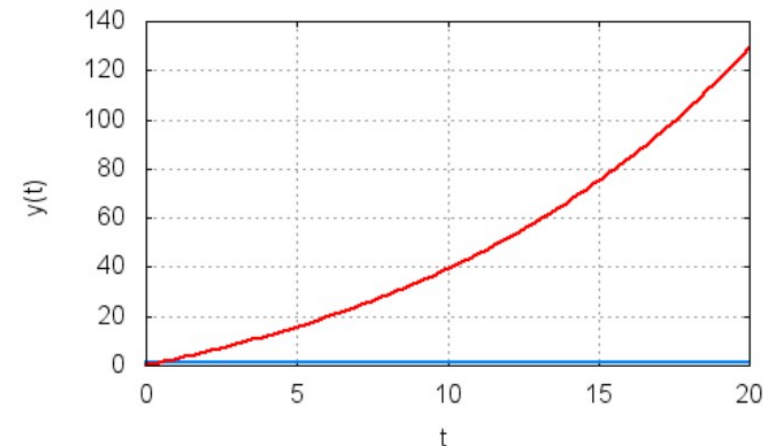


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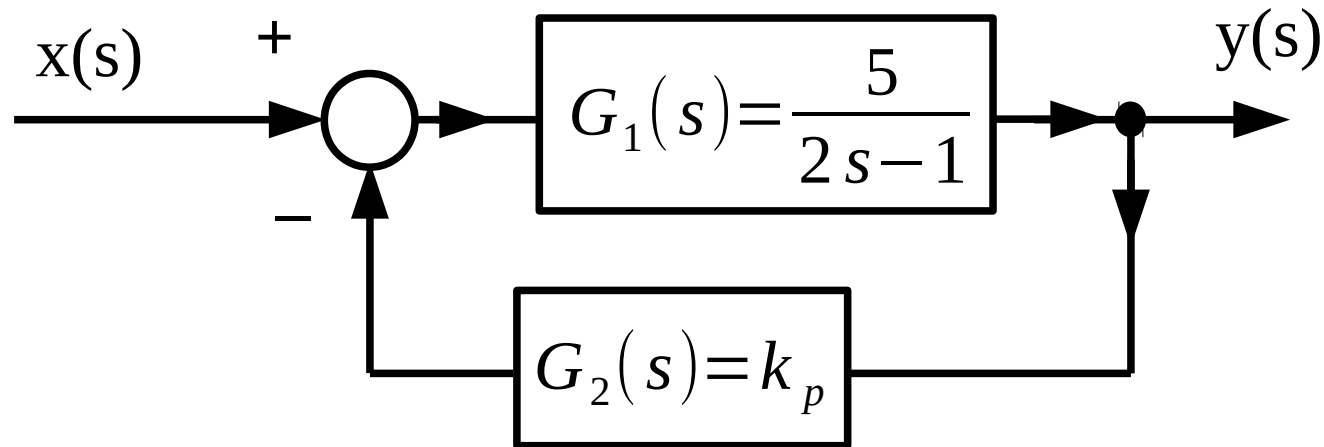
System is stable, if  $\Re(p_1) < 0 \Rightarrow k_p > \frac{1}{5}$

$k_p = \frac{1}{6}$  (unstable)



## Example 2

Choose values of  $K_p$  to obtain system stability using the general stability criterion

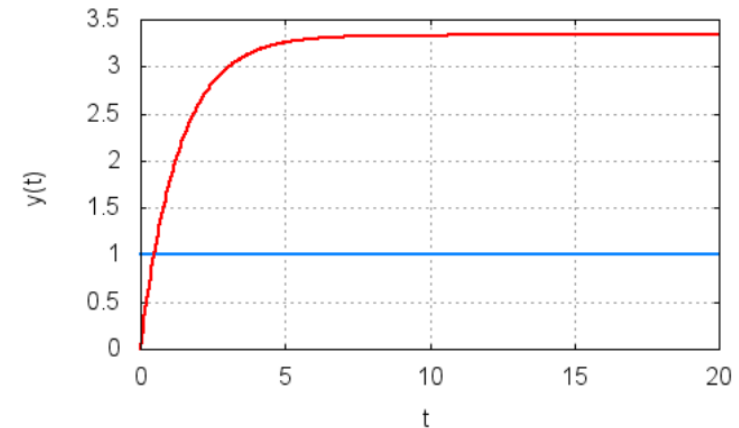


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$$p_1 = \left( \frac{1}{2} - \frac{5}{2} k_p \right)$$

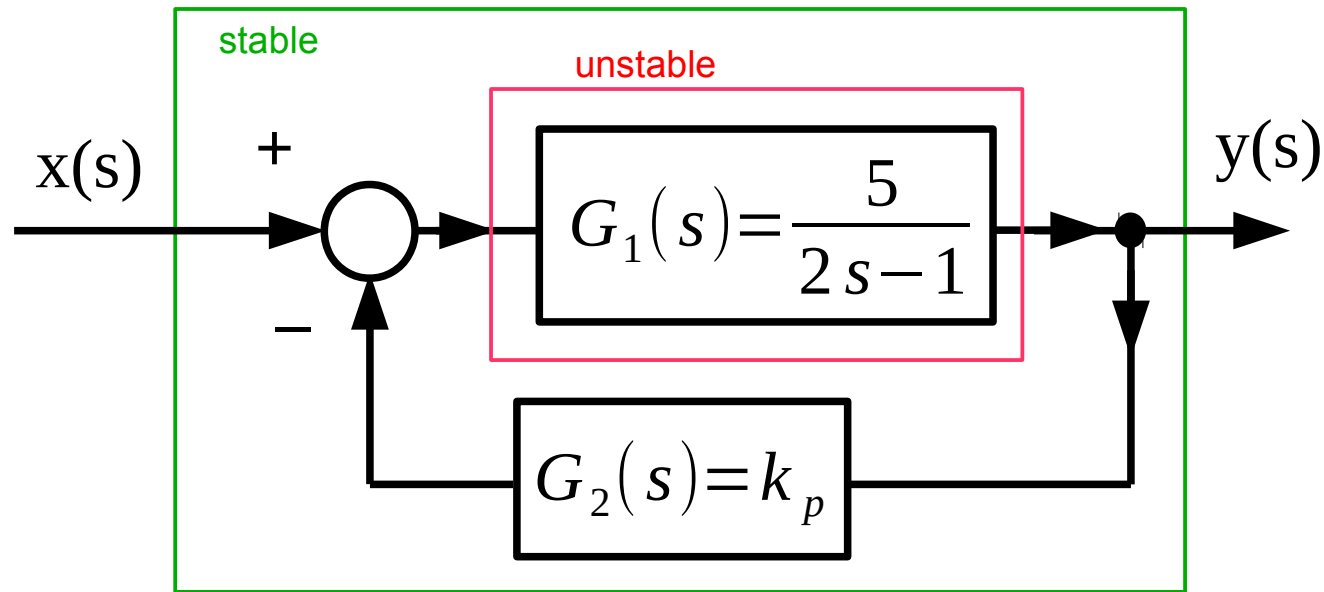
System is stable, if  $\Re(p_1) < 0 \Rightarrow k_p > \frac{1}{5}$

$k_p = \frac{1}{2}$  (stable)



# Example 2

Choose values of  $K_p$  to obtain system stability using the general stability criterion

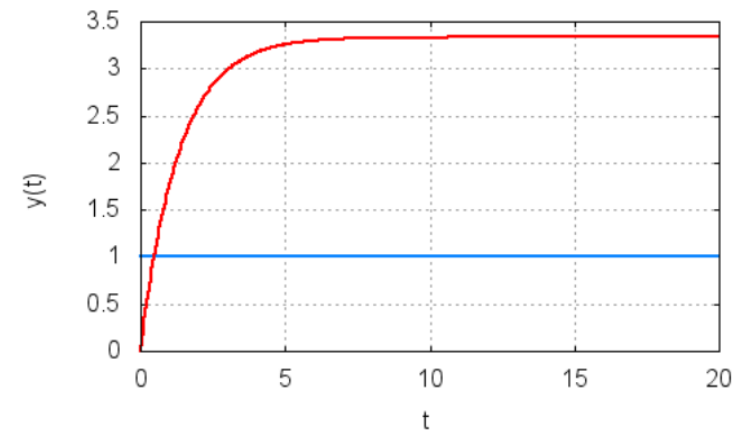


$$G(s) = \frac{Y(s)}{X(s)} = \frac{G_1}{1 + G_1 G_2} = \frac{5}{2} \frac{1}{s - \left( \frac{1}{2} - \frac{5}{2} k_p \right)}$$

$$p_1 = \left( \frac{1}{2} - \frac{5}{2} k_p \right)$$

System is stable, if  $\Re(p_1) < 0 \Rightarrow k_p > \frac{1}{5}$

$k_p = \frac{1}{2}$  (stable)



# List of important exam topics

- Mechanism mobility calculation
  - Procedure analytical method
  - Equation of machine motion
    - Nonuniformity and flyweel
- Transfer function of LTI SISO
- Step response & Bode Plot of a given system
  - Block diagram algebra
  - PID controller & tuning
  - General stability criterion
    - Hurwitz criterion
  - particular Nyquist criterion